

EDF R&D



FLUID DYNAMICS, POWER GENERATION AND ENVIRONMENT DEPARTMENT
SINGLE PHASE THERMAL-HYDRAULICS GROUP

6, QUAI WATIER
F-78401 CHATOU CEDEX

TEL: 33 1 30 87 75 40
FAX: 33 1 30 87 79 16

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code_saturne documentation

**code_saturne version 8.0 tutorial:
Heated Square Cavity Flow**

contact: saturne-support@edf.fr



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Chapter I

Introduction

1 Tutorial Components

This tutorial makes use of:

- The SALOME [1] platform for geometry generation, meshing, and post-processing
- code_saturne [2, 3] for CFD calculations
- References [4, 5, 6] for comparison with published results

To work through this tutorial you will need a computer on which these two software applications are already available or on which you have permission to install them.

You will also need to know how to create and setup a code_saturne case with the CFDStudy module. For instructions on how to do so, please see [7].

2 Tutorial Structure

This tutorial is made of two complementary parts:

- Part 1 (Section II) illustrates how to setup, conduct and analyse a natural buoyancy CFD simulation with temperature-dependent density using SALOME and code_saturne and its user-defined functions.
- Part 2 (Section III) illustrates how the user subroutine ‘cs_user_extra_operations.f90’ may be used to compute additional custom data from the calculated data in order to analyse a simulation and compare its results with published data.

If you are already familiar with setting up CFD simulations with code_saturne and SALOME and you only want to learn how to compute custom data with ‘cs_user_extra_operations.f90’, you may skip Part 1 and go directly to Part 2 (Section III).

Chapter II

Part 1 - Heated Square Cavity Flow CFD Study

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The preparation, simulation and analysis of the ‘Rayleigh1Million’ case of the ‘HeatedSquareCavity’ study are described in section II, from the construction of the computational domain and mesh to the preparation, running and post-processing of the CFD simulation.

A familiarity with C programming would be desirable to understand the user coding in detail, however it is not strictly a requirement as the user subroutines may be used in the form delivered with this tutorial.

1 What You Will Learn

Through this tutorial, you will learn how to perform an end-to-end CFD simulation using SALOME and code_saturne. The tutorial illustrates how to:

- Create a computational domain using available shapes and groups
- Create an hexahedral mesh with different mesh refinement in the X, Y and Z directions
- Setup a code_saturne [2, 3] steady-state, viscous, laminar CFD simulation with
 - Buoyancy
 - Heat transfer
 - Variable density
 - Non-slip walls with a combination of imposed heat flux and temperature
 - Symmetry planes
- Model natural convection with the Boussinesq approximation and gravity
- Program user subroutines to:
 - Model the density as a function of temperature
 - Compute user defined variables and extract quantities of interest for post-processing
- Control and run the code_saturne simulation
- Examine the code_saturne output and results files
- Analyse and visualise the results
- Visually and quantitatively compare the case results with available data

2 Case Description

The tutorial refers to the classic natural convection benchmark cases of de Vahl Davies and co-workers [4, 5, 6].

A viscous fluid is contained in a two-dimensional square box, or cavity (Figure II.1). All the walls of the cavity are fixed. Whilst the horizontal walls are **isolated and adiabatic** (zero heat flux), the vertical walls are kept at **constant temperature**. The left vertical wall is the **hot wall**, with a fixed temperature of T_h . The right vertical wall is the **cold wall**, with a fixed temperature of T_c .

The acceleration of gravity points downward in the vertical (y-axis) direction.

The temperature values form part of the specification of the problem and are specified in Sections 2.3 and 2.5 along with the box’s dimension for this tutorial.

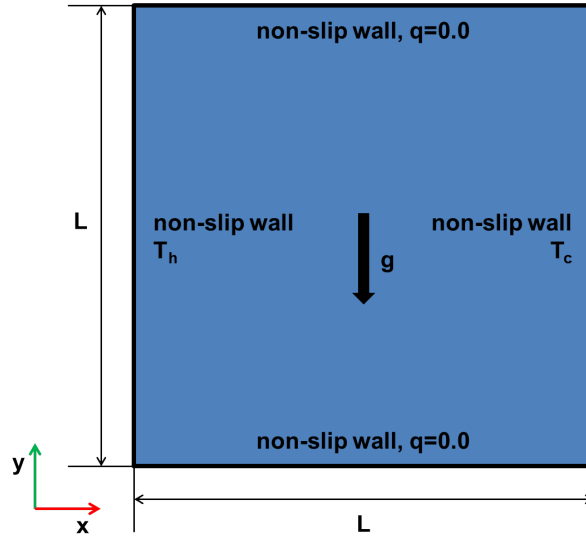


Figure II.1: Schematic of the 2D Heated Square Cavity.

The flow physics are described next.

2.1 Flow Physics

The problem is setup to simulate the natural convection of a fluid in the presence of a body force (gravity) as it changes density with temperature. In this example, a basic pattern is obtained where the fluid rises along the hot wall, is driven by its momentum along the top wall and towards the cold wall where it cools down and moves downwards. More or less complex flow patterns may be obtained depending on the size of the cavity, the fluid properties, and the temperature difference between the two walls.

The dominant physics of the problem being buoyancy and heat transfer, the problem may be characterised in terms of the Rayleigh number based on the cavity size, defined as the product of the Prandtl and Grashof numbers:

$$Ra = Pr Gr = \frac{\mu C_p}{k} \cdot \frac{g \beta (\Delta T) L^3}{\nu^2} = \frac{\rho^2 C_p g \beta (\Delta T) L^3}{k \mu} \quad (\text{II.1})$$

where ρ is the density, C_p is the specific heat at constant pressure, g is the acceleration of gravity, β is the thermal expansion coefficient defined as $\beta = -\frac{1}{\rho} \left(\frac{\partial \rho}{\partial T} \right)_p$, ΔT is the characteristic temperature difference, k is the thermal conductivity, and μ is the viscosity. In this problem, $\Delta T = T_h - T_c$, the temperature difference between the heated walls of cavity.

The flow patterns and characteristics of the heated cavity, such as velocity extremas and heat fluxes, can all be classified as functions of the Ra number. Turbulent flow occurs when $Ra \geq 10^9$.

For the purpose of this tutorial, you will perform laminar flow simulations for $Ra = 10^6$ and compare the results to the laminar flow benchmarks of de Vahl Davis et al. [5, 6]. In this regime, the flow is essentially incompressible. However, variations of density with temperature must be taken into account in order to simulate buoyancy. This combination of an incompressible fluid assumption with a density variation explicit in the gravitational term is known as the Boussinesq approximation [9], which is described next.

2.2 Boussinesq Buoyancy Approximation - Theory

Applying the definition of the thermal expansion coefficient to a perfect gas:

$$\left(\frac{\partial \rho}{\partial T}\right)_p = -\frac{p}{RT^2} = -\frac{p}{T} \rightarrow \beta = \frac{1}{T} \quad (\text{II.2})$$

With the Boussinesq approximation, the density is calculated as a function of temperature, with respect to the reference state (ρ_0, T_0) :

$$\rho - \rho_0 = -\rho_0 \beta_0 (T - T_0) \quad \beta_0 = \frac{1}{T_0} \quad (\text{II.3})$$

This density formulation is not already coded in code_saturne. Instead, you will need to program it in user subroutine `cs_user_physical_properties.c`, as described in Sections 2.7 and 5 below.

2.3 Geometry

The cavity is a square of length $L = 1.0$ (m).

2.4 Fluid Properties

The fluid is given the properties of air, specified at the cold wall temperature, T_c , as listed in Table II.1 below.

Density (kg/m ³)	Viscosity (Pa.s)	Specific Heat (J/kg.K)	Thermal Conductivity (W/m.K)
1.2039	1.83×10^{-5}	1004.84	0.0259

Table II.1: Fluid Properties.

The properties are calculated for a perfect gas at the reference state of $T = 293.15K$ and $P = 101325Pa$, with $\gamma = 1.4$ and to ensure that $P_r = 0.71$, as per the benchmark specifications.

2.5 Boundary Conditions

As described in above, the domain is fully enclosed by non-slip walls. This means that, exactly at the surface of the walls, the fluid inside the box attaches to the walls and has exactly the same velocity as the walls. Therefore, for the momentum equations, the problem is fully defined by specifying that all the walls are fixed. For the energy equation, the two vertical walls are kept at constant temperature whilst the horizontal walls are adiabatic. The boundary conditions are summarised in Table II.2 below.

Wall	Velocity component(m/s)		Energy	
	v_x	v_y	T(K)	Q(J/m ²)
Left	0.0	0.0	303.15	N/A
Top	0.0	0.0	N/A	0.0
Right	0.0	0.0	293.15	N/A
Bottom	0.0	0.0	N/A	0.0

Table II.2: Wall boundary conditions.

The temperature difference between the two walls is kept under 20 (K) which ensures the validity of the Boussinesq approximation.

2.6 Flow Regime

For this tutorial, the setup is chosen so that $R_a = 10^6$, for which the flow is steady and laminar . This Rayleigh number corresponds to the highest Rayleigh number reported in [5, 6] making comparisons with benchmark results possible and ensuring significant fluid motion in the cavity and complex flow patterns.

2.7 Boussinesq Buoyancy Approximation – code_saturne Formulation

As the Boussinesq approximation is not directly available in code_saturne, it will need to be implemented with **user code**. The actual programming of user subroutine 'cs_user_physical_properties.c' for this purpose is described in Section 5. Here, we describe the formulation chosen for this tutorial.

The reference state is taken at the cold wall temperature. Therefore, the density law becomes:

$$\rho = \rho_c(1 - \beta(T - T_c)) \quad (\text{II.4})$$

Further, in order to make the simulations flexible, in this tutorial we make β a variable of the imposed Rayleigh number, instead of using the physical definition of β as derived for a perfect gas:

$$\beta = \frac{k\mu}{\rho^2 C_p g (T_h - T_c) L^3} R_a \quad (\text{II.5})$$

This way, it will be possible to simulate the flow for different Rayleigh numbers just by changing the value of the imposed Rayleigh number in the user subroutine and without altering the geometric or physical setup.

3 Creating the code_saturne case

The 'HeatedSquareCavity' study and 'Rayleigh1Million' case are created using one of the procedures detailed either in Part I of tutorial 0 [7] (or Figure II.2) or tutorial 1 [8]

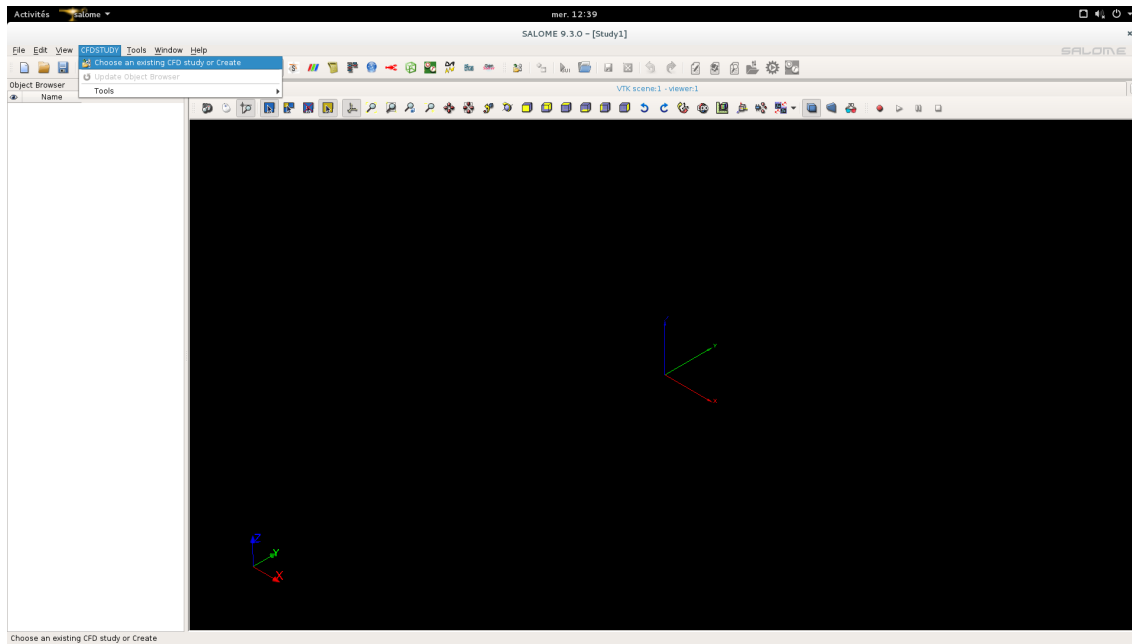


Figure II.2: New study in CFDSSTUDY.

The next sections describe how to setup and run the heated cavity simulation for a Rayleigh number of 10^6 .

4 Setting up the CFD Simulation

The CFD case could be setup using either SALOME CFDSStudy module or code_saturne. In this tutorial code_saturne is used. Open the code_saturne GUI and follow the next steps. In the code_saturne GUI, create a new code_saturne xml file with 'New File'. Verify that the case directory structure has been recognised and save the file. The default name is 'setup.xml'.

You can now proceed with to the set up of code_saturne case, in the top down order of the folders in the left-hand side, starting with the mesh.

4.1 Mesh Tab

You could either import meshes or generate cartesian mesh if you previously skipped Meshing creation part.

Option 1 - Import meshes In the 'Mesh' section add the 'HSC_mesh.med' to the initially empty list of meshes (Figure II.3).

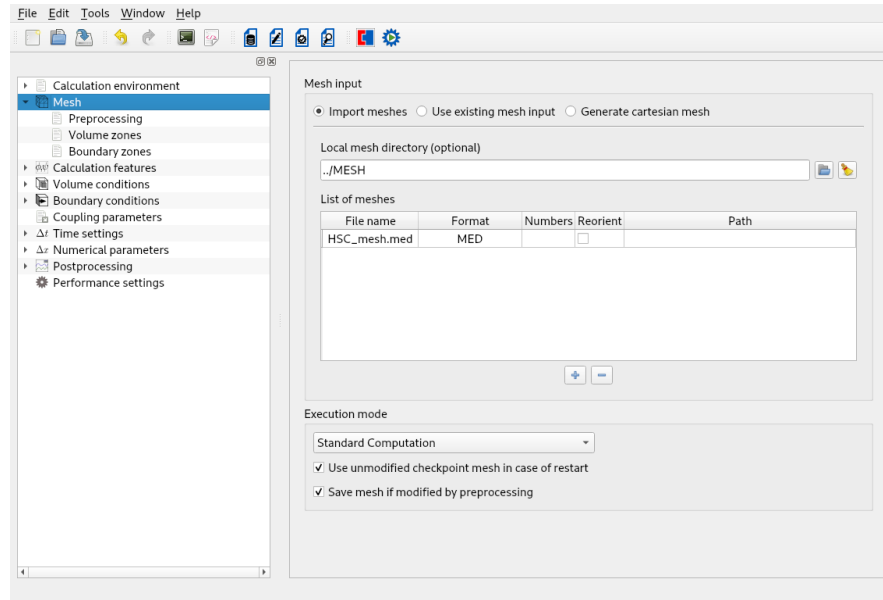


Figure II.3: Selecting the 'HSC_Mesh.med' file for the calculations.

Option 2 - Generate cartesian mesh This code_saturne version allows users to generate parallelepipedal cartesian mesh. This case is compatible with such option. To do so you can select *Generate cartesian mesh*, fill all fields for every direction as follows :

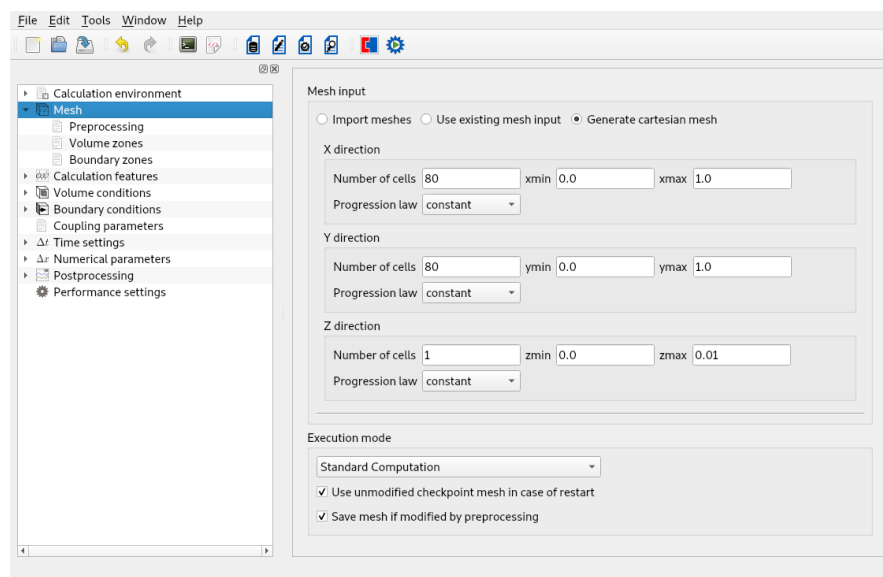


Figure II.4: Cartesian mesh generation

Boundary zones Under the 'Boundary zones' section, press 'add' three times to add three boundary conditions which are given the 'Wall' type by default. Change the name of each wall to reflect exactly the name of each of the walls in the mesh: 'hot_wall', 'cold_wall', and 'adiabatic_walls'. Boundary zones are now fully defined (Figure II.6). **Option 1 - Import meshes**

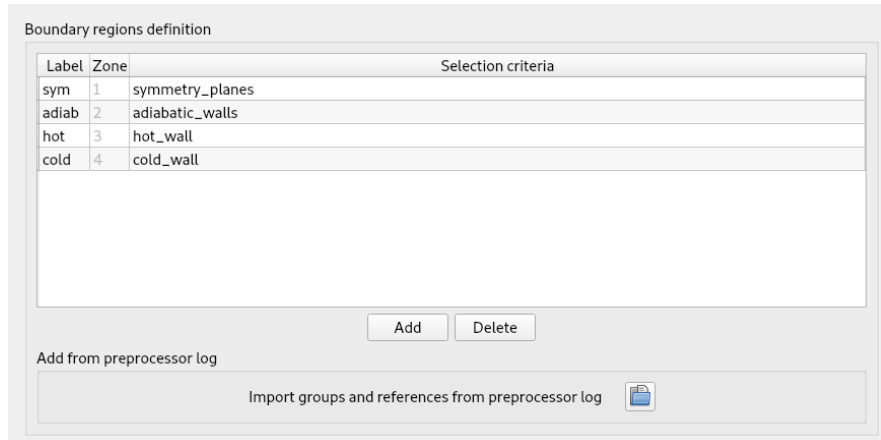


Figure II.5: Defining the boundary conditions if mesh is imported

Option 2 - Generate cartesian mesh

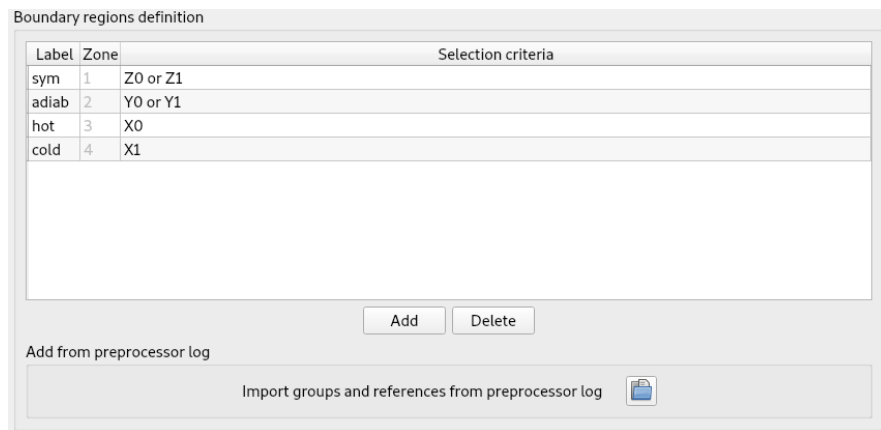


Figure II.6: Defining the boundary conditions if mesh is generated via code_saturne alternativ method

Note: If you need to define boundary faces in the selection criteria fields you can use the following abbreviation. X0 refers to the face normal to X axis with the lowest coordinate while X1 refers to the face normal to X axis with the highest coordinate.

	X	Y	Z
Min	X0	Y0	Z0
Max	X1	Y1	Z1

No further input is necessary. Next, move to 'Calculation features' to specify the flow physics for the calculations.

4.2 Calculation features Tab

In the 'Calculation features' folder, leave all the default values unchanged: multiphase flow, atmospheric flows, combustion and the electrical and compressible models are all inactive.

Turbulence models Next, change 'Turbulence model' to 'No model' for this laminar flow case.

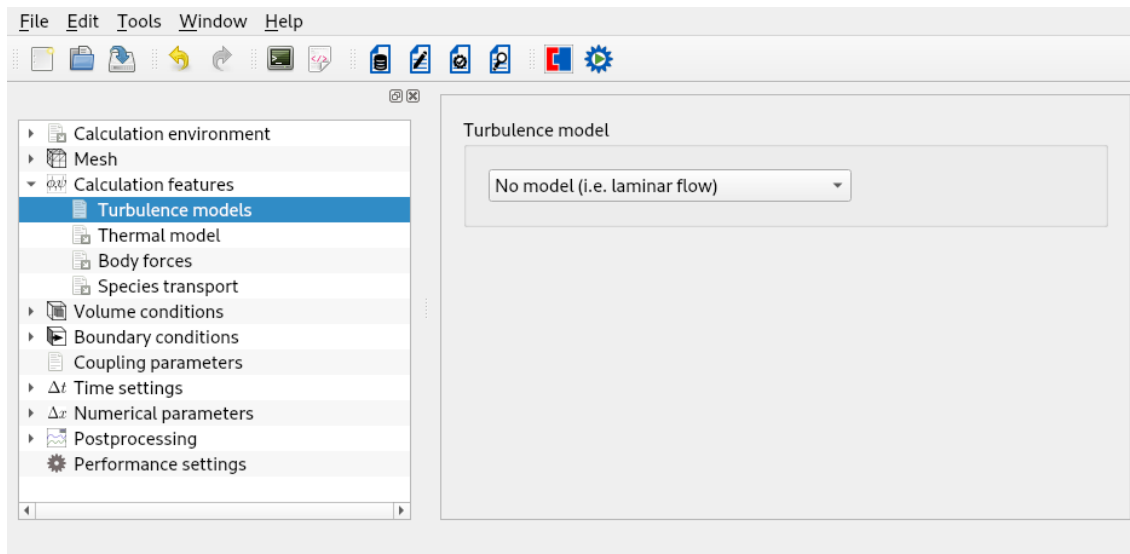


Figure II.7: Deactivating turbulence model

Thermal model In this section, choose 'Temperature (Kelvin)' for the 'Thermal scalar'. This will activate solution of the energy equation and designate Temperature as the scalar specified at the boundary conditions (Figure II.8).

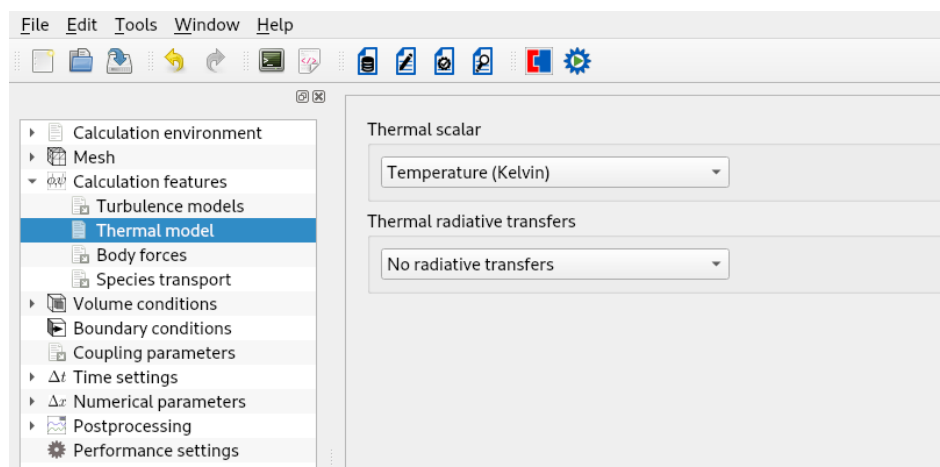


Figure II.8: Activating solution of the energy equation.

Body forces Go to the 'Body forces' section in order to activate the acceleration of gravity by entering the value magnitude ' -9.81m/s^2 ' for its component in the vertical (Y) direction (Figure II.9).

The image shows a configuration window for gravity and Coriolis source terms. It contains two main sections: 'Gravity' and 'Coriolis source terms (rotation vector)'. Each section has three input fields for the x, y, and z components, each with a unit of m/s^2 or s^{-1} .

Section	Component	Value	Unit
Gravity	g_x	0.0	m/s^2
	g_y	-9.81	m/s^2
	g_z	0.0	m/s^2
Coriolis source terms (rotation vector)	Ω_x	0.0	s^{-1}
	Ω_y	0.0	s^{-1}
	Ω_z	0.0	s^{-1}

Figure II.9: Specifying gravity.

4.3 Volume conditions Tab

Physical properties You can specify the properties of our imaginary fluid by entering all values from Table II.1 above in the text boxes (Figure II.12). Density parameters declared in the GUI will be overwritten by the user subroutine 'cs_user_physical_properties'. So you can leave density parameters as follows.

The image shows the 'Physical properties' tab in the software interface. The left sidebar shows a tree view with 'Volume conditions' expanded to 'all_cells'. The main panel contains several sections for defining fluid properties:

- Material:** user_material
- Method:** user_properties
- Reference total pressure:** value 101325.0 Pa
- Reference temperature:** value 293.15 K (used for properties initialization)
- Density:** constant, Reference value ρ 1.2039 kg/m^3
- Viscosity:** constant, Reference value μ 1.83e-05 Pa.s
- Specific heat:** constant, Reference value C_p 1004.84 J/kg/K
- Thermal conductivity:** constant, Reference value λ 0.0259 W/m/K

Figure II.10: Selecting fluid physical properties.

Initialization Velocity and temperature initial values are defined in the *'Initialization'* tab of the **'Volume zones'** section. The flow is initially stagnant by default. To set the initial temperature, click on the Mathematical Expression Editor button marked *'Thermal'* and enter the temperature of the cold wall (Table II.2) in the pop-up editor panel (Figure II.11).

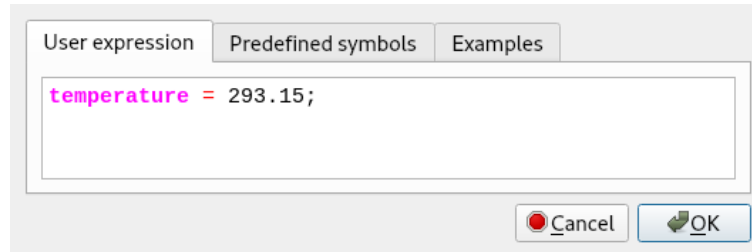


Figure II.11: Specifying the initial temperature.

4.4 Boundary conditions Tab

You need to define nature for all boundary zones as follows :



Figure II.12: Assigning boundary zone nature.

Where required depending on the boundary type, the conditions applied on the region must also be specified under the *'Boundary Conditions'* sub-section of *'Boundary zones'*.

Boundaries of type *'Symmetry'* do not require further specification. Therefore, they are not listed in this section. However, *'Walls'*, may also be given a surface roughness, velocity (sliding wall) and thermal characteristics (either heat flux or temperature).

By default, *'Walls'* are assumed to be smooth, fixed, and adiabatic. Therefore, no further changes are required for boundary *'adiabatic-wall'*, as shown in Figure II.13(left) below. For the heated vertical walls, click on each wall in succession, specify *'Prescribed value'* for the type and enter the imposed temperature in *'Value'* according to Table II.2 and as illustrated for the *'hot-wall'* boundary in Figure II.13(right) below.

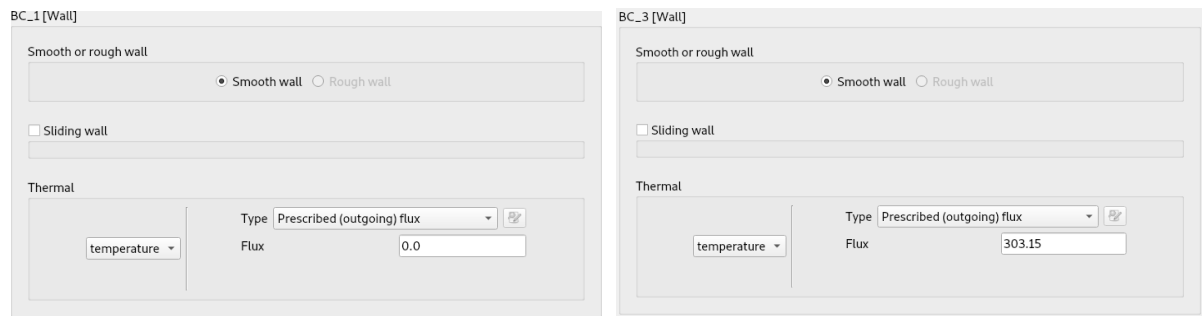


Figure II.13: Specifying the wall boundaries. Adiabatic wall (left), Hot wall (right).

4.5 Time settings Tab

In the ‘**Time settings**’ section, change **Constant** to **Time varying (adaptive)** at the **Time step option**. Then, increase the ‘*Number of time steps*’ to **450** and the ‘*Maximal CFL number*’ to **8.0**. leave all the other values unchanged.

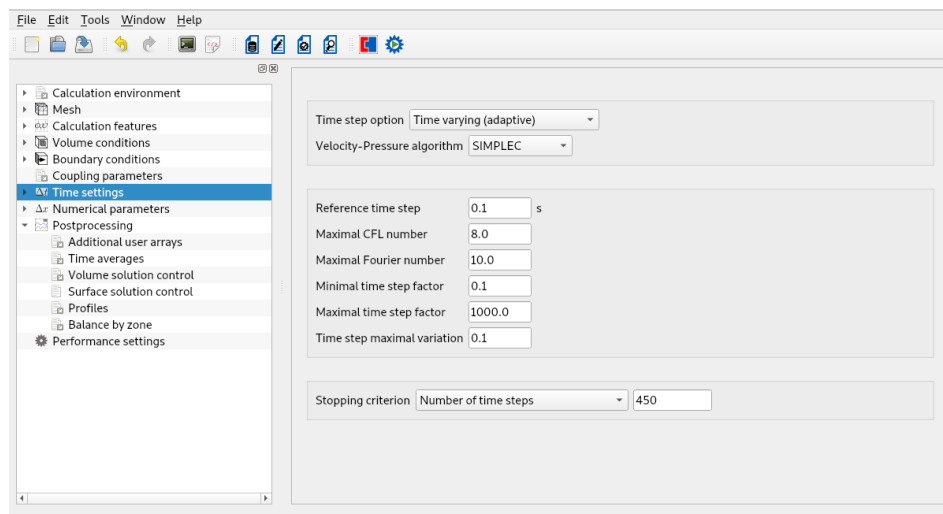


Figure II.14: Defining Time settings

4.6 Numerical parameters Tab

Leave all the default settings in the ‘**Numerical Parameters**’ section.

Move to the ‘**Equation parameters**’ sub-section. The ‘**Solver**’ tab shows that pressure, velocity and temperature are solved for. Click on the ‘*Scheme*’ tab. For better convergence, and as the flow in the cavity will involve small temperature and density variations, keep the ‘**Centered**’ scheme for all variables but unselect the ‘**Slope test**’ (Figure II.15).

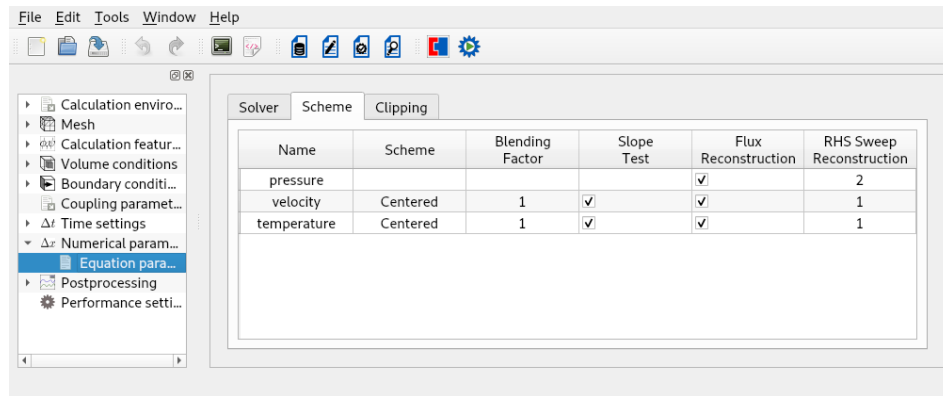


Figure II.15: Defining the numerical schemes.

The ‘Clipping’ tab is used to set the temperature bounds, making it possible to instruct the code to clip the temperature to these values if it strays outside the defined range. This feature can be very useful to prevent spurious, low or high values, from poisoning a calculation, for example when convergence has not yet been achieved. However, it is not required for this tutorial and you may leave the default values unchanged.

4.7 Postprocessing Tab

Surface solution control : Unselect ‘Yplus’, ‘Stress’, and ‘Tplus’ from the list of variables to output on surfaces as they are not relevant to this tutorial. Note that both ‘Thermal flux’ and ‘Boundary temperature’ have been automatically added to the list when the thermal model was activated. Add ‘Boundary layer Nusselt’ to the selection (Figure II.16) and save the file.

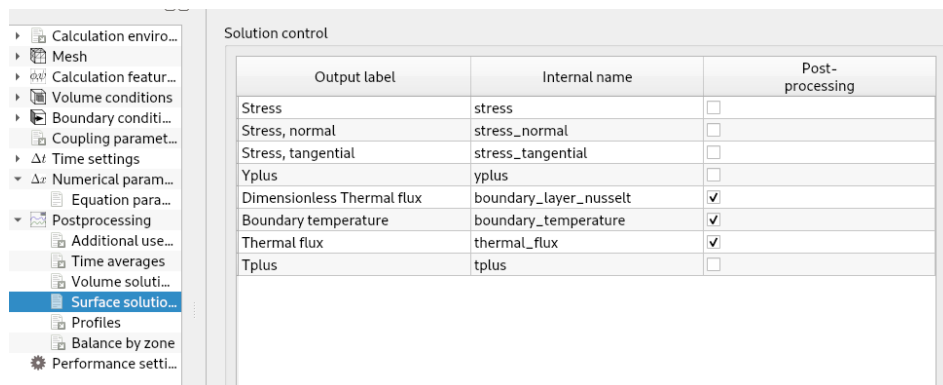


Figure II.16: Defining the output variables on surfaces.

The analysis of the wall and domain data will be done in user coding as described in section III below and no further specification of ‘Time averages’, ‘Output control’ and ‘Profiles’ is required.

The code_saturne calculation is now fully specified from the standpoint of the GUI and the file should be saved again. However, before you can run the simulation, the density law must be programmed in the user coding file ‘cs_user_physical_properties.c’. This step is described next.

5 Programming the Boussinesq Model with User Coding


To begin with, copy the sample file ‘cs_user_physical_properties.c’ from the tutorial’s `../HeatedSquareCavity/Rayleigh1Million/SRC/REFERENCE` directory to the SRC directory itself in order to create a local copy which you will be able to customise and which will be automatically recompiled and linked with the ‘cs_solver’ executable at run time.

Then, open your local version of the file in your editor of choice.

The files contain a number of subroutines. The specification of a physical property is done in subroutine ‘cs_user_physical_properties’. Scrolling through this subroutine, you can see that several examples of implementations for different physical properties are available. In this tutorial, you are going to amend ‘Example 1’ with your own implementation of the density as a function of temperature (equations (II.4) and (II.5)). For clarity, you may remove all the other examples from the file. The customised code available with the tutorial is already commented. Here we describe the main parts and the logic behind them.

1. Declare your own local variables at the top, as double precision real values or integer.
2. Activate the example (replace ‘.false.’ with ‘.true.’)
3. Specify the desired Rayleigh number for the simulation
4. Compute the magnitude of the gravity vector from the information entered in the CFDStudy module
5. Impose the domain size and wall temperatures consistently with the problem setup
6. Compute the expansion coefficient for the physical properties entered in the CFDStudy module and the imposed Rayleigh number
7. Cycling through the internal cells of the computational domain:
 - (a) Compute the density as a function of temperature, using the cold wall temperature and density as the reference state
 - (b) Compute the density maxima and minima for output purposes
8. Write the values of the density maxima and minima to the output file ‘listing’ with the keyword ‘cs_user_physical_properties’ for easy identification

6 Running and Analysing the Simulation

To launch the simulation, click on the  button.

A new window will open allowing you to specify some calculation options (Figure II.17). Here, you can change the ‘Number of processes’ to those that you require for running the simulation.

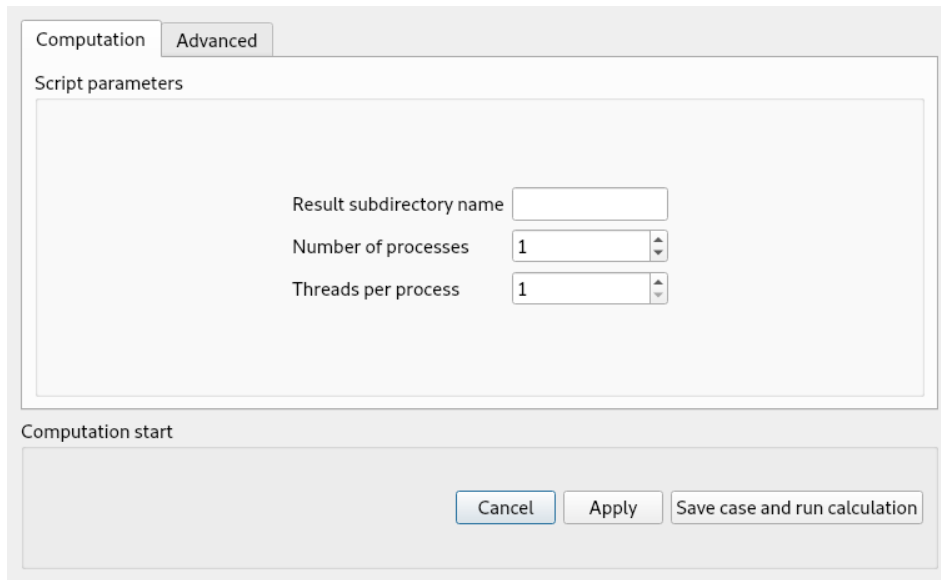


Figure II.17: Batch calculation settings.

After specifying ‘Number of processes’, press the ‘Save case and run calculation’ button to run the simulation.

The pop-up panel for the run opens, listing in real time the different stages of the calculation, from user-subroutines compilation to saving the results.

Wait for the calculations to complete and open the ‘listing’ file in your ‘Rayleigh1Million/RESU/DateOfRunTimeOfRun/’ directory. Verify that the residuals listed under ‘derive’ in the ‘Information on Convergence’ table have dropped several order of magnitudes for all the solved variables (pressure, velocity, temperature), showing that the calculations have fully converged to a steady-state.

```

** INFORMATION ON CONVERGENCE
-----

```

Variable	Rhs norm	N_iter	Norm. residual	Drift	Time residual
c Velocity	0.00000E+00	0	0.00000E+00	0.00000E+00	0.00000E+00
c Velocity[X]				0.00000E+00	
c Velocity[Y]				0.00000E+00	
c Velocity[Z]				0.00000E+00	
c Pressure	0.00000E+00	0	0.00000E+00	-0.00000E+00	0.00000E+00
c TempK	0.40330E+03	1	0.33350E-07	0.94543E-02	0.10001E-02

```

-----

```

Figure II.18: code_saturne Convergence history from the ‘listing’ file, after 1 iteration.

** INFORMATION ON CONVERGENCE

```

-----
Variable                Rhs norm      N_iter  Norm. residual  Drift  Time residual
-----
c Velocity              0.14335E-07    7   0.93548E-05   0.99286E-15  0.45550E-05
c Velocity[X]                    0.55852E-15
c Velocity[Y]                    0.43434E-15
c Velocity[Z]                    0.42593E-15
c Pressure              0.47414E-09    9   0.10387E-07   0.60185E-04  0.41853E-05
c TempK                 0.31390E+01    1   0.27810E-05   0.77969E-08  0.64957E-07
-----

```

Figure II.19: code_saturne Convergence history from the 'listing' file, after 450 iterations.

Scanning through the listing file for the 'cs_user_physical_properties' output, inspect how the density has changed during the calculations, to verify that the user-code has been called and validate your implementation. As required, the density has decreased as a consequence of the temperature of the fluid increasing next to the hot wall.

```

INSTANT    0.100000000E+00  TIME STEP NUMBER          1
=====

rho_min =    1.2038999999756232      , rho_max =    1.2038999999756232

```

Figure II.20: code_saturne Density extremas history from the 'listing' file, after 1 iteration.

```

INSTANT    0.450000000E+02  TIME STEP NUMBER          450
=====

rho_min =    1.2038603236819787      , rho_max =    1.2038997567079919

```

Figure II.21: code_saturne Density extremas history from the 'listing' file, after 400 iterations.

You can now proceed with examining and post-processing the results by returning to the SALOME platform.

7 Post-processing the Results

The post-processing is performed with the ParaView [10] visualisation package, which is integrated in the ParaVis SALOME module. To start the analysis, select the ParaVis module from the drop-down module selector in the top menu bar. The name of the module will add itself to the Object Browser list and the ParaView-specific panels and menus will be activated, including a new 'ParaView scene viewer' window.

Before loading the run data in ParaView, follow the steps described in Tutorial 1, Part 2 [7] to modify the default colour schemes.

In the 'Pipeline Browser' panel on the left-hand side, right click and select 'Open' in the drop-down menu. Point to the 'RESULTS_FLUID_DOMAIN.case' file in the RESU directory for the run you have just concluded:

../Rayleigh1Million/RESU/DateOfRunTimeOfRun/postprocessing/RESULTS_FLUID_DOMAIN.case.

The new Paraview object 'RESULTS_FLUID_DOMAIN.case' will now become visible in the 'Pipeline Browser'.

To visualise the results and compare them qualitatively to the benchmarks of [5, 6], you will need to create isoline contours of temperature and streamlines which show the flow patterns. To create these plots, the data output by code_saturne given at the centres of the cells first needs to be interpolated to the cell vertices. As described in Tutorial 1, Part 2 [7], with 'RESULTS_FLUID_DOMAIN.case' selected, in 'Filters' at the top of the Paraview window, select the 'CellDatatoPointData' filter, which will create the 'CellDatatoPointData1' object. Click on the object and select 'Contours' in the list of filters. Again this will create a new object based on its originator, this time name 'Contour1' (Figure II.22).

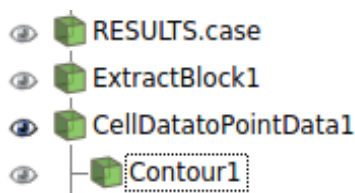


Figure II.22: The chain of Paraview visualisation objects.

To create the temperature isolines, click on 'Contour1' and click on 'Apply' in its 'Object Inspector' 'Properties' tab. Choose 'TempK' in the 'Contour' category as shown in Figure II.23 below.

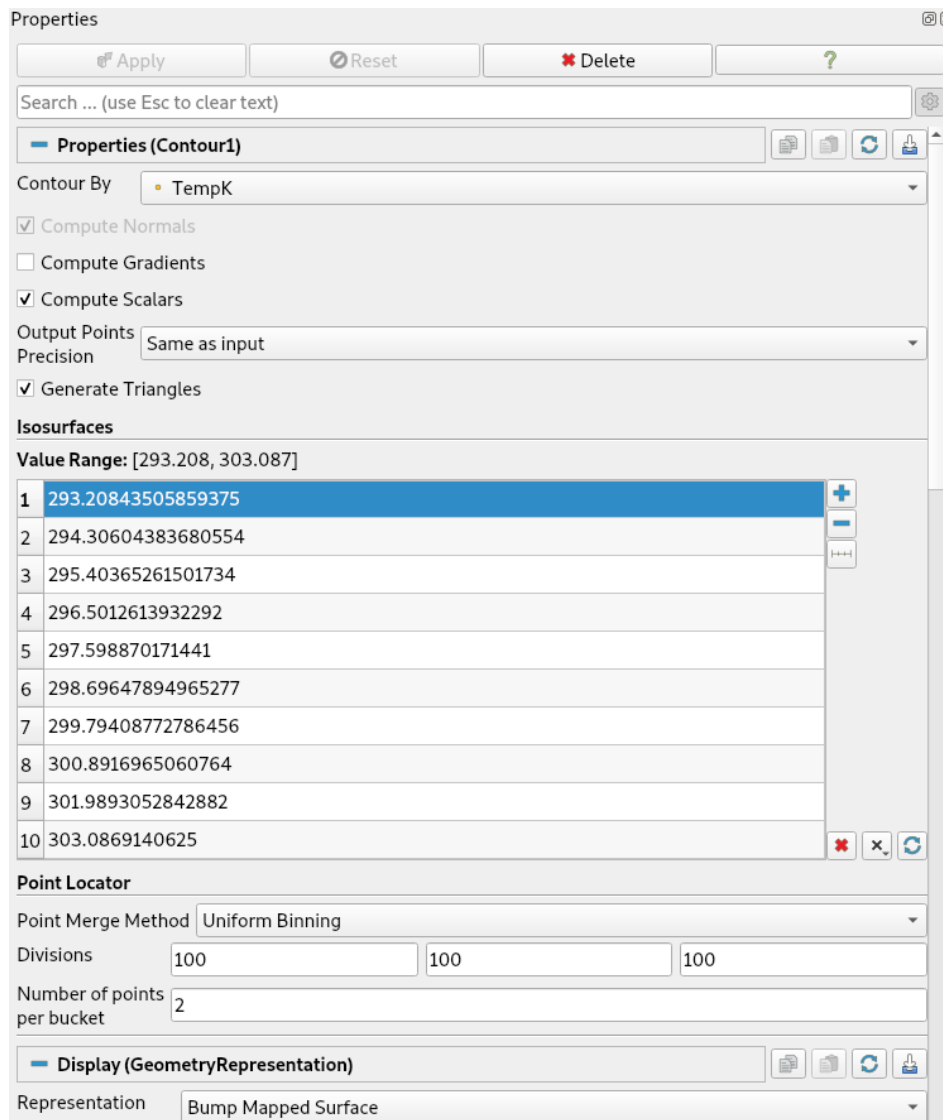


Figure II.23: Specifying the temperature isolines in the Contour filter.

In the 'Isosurfaces' category, press 'Delete All' to reset the contour levels. Then press 'New Range' and specify 11 levels in the pop-up window in order to display the same number of isolines as in the plots published in [5], [6]. The correct value range should already be set in the panel. For better rendering, the colour scale should be changed to the 'Blue to Red' 'HSV' in the 'Display' tab, as per the instructions of Tutorial 1, Part 2 [7]. Add the colour scale to the plot by clicking on its icon on the left of the top Paraview menu bar.

To complete the image, we want to superimpose the contour lines on top of the computational domain. Select 'CellDataToPointData1' and 'Solid Color' for the display. Change the representation from 'Surface' to 'Outline' to visualise the cavity's perimeter. Make sure that the icon in the form of an eye to the left of 'CellDataToPointData1' is active for the object to be visible. If the isolines have become invisible, unclick on the eye icons on the 'Contour1' and 'CellDatatoPointData1' objects, then make them visible again starting with 'CellDatatoPointData1' to keep it in the background.

A plot of 9 visible isolines of temperature is then obtained which compares very well with the published results of [5], [6] (Figure II.24). If required, reset the temperature scale manually for the bounds to match exactly the range of the isolines (Figure II.23).

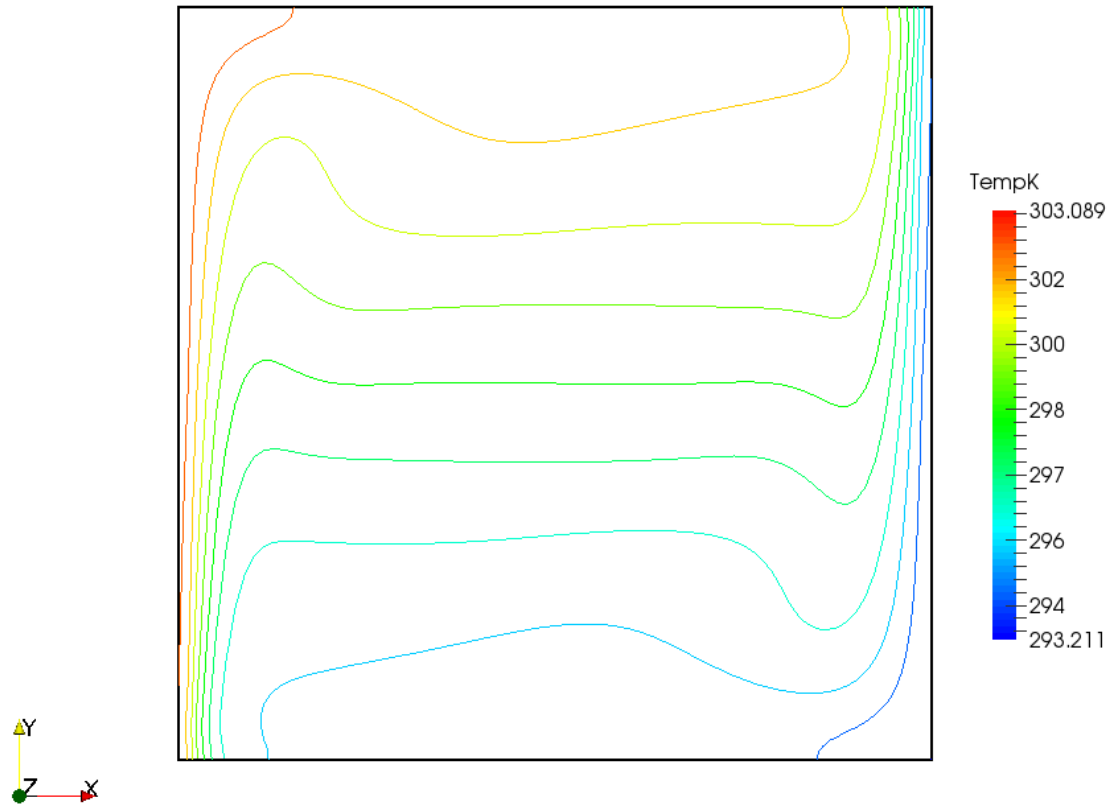


Figure II.24: Temperature isolines.

Next, prepare a visualisation of the streamlines which can also be compared directly with the benchmark results. The procedure to generate streamlines superimposed on a view of the computational domain has already been described in Tutorial 1, Part 2 [7] and only the features specific to this tutorial are detailed here.

With 'CellDatatoPointData1' selected in the Pipeline Browser, choose 'Steam tracer' from the 'Filters' list. Select the 'StreamTracer1' object in the Pipeline Browser and make it visible. In the 'Object Inspector', select the 'Properties' tab and modify the default settings for 'Seeds'. Change 'Point Source' to 'Line Source'. The diagonal line showing the location of the streamline seeds becomes visible in the visualisation window. For the purpose of post-processing, unselect 'Show Line' under 'Seed Type'. In the 'Display' tab, choose 'Velocity' and 'Magnitude' in the 'Color' sub-category. The streamlines show the expected flow symmetry and very good agreement with the published benchmarks (Figure II.25).

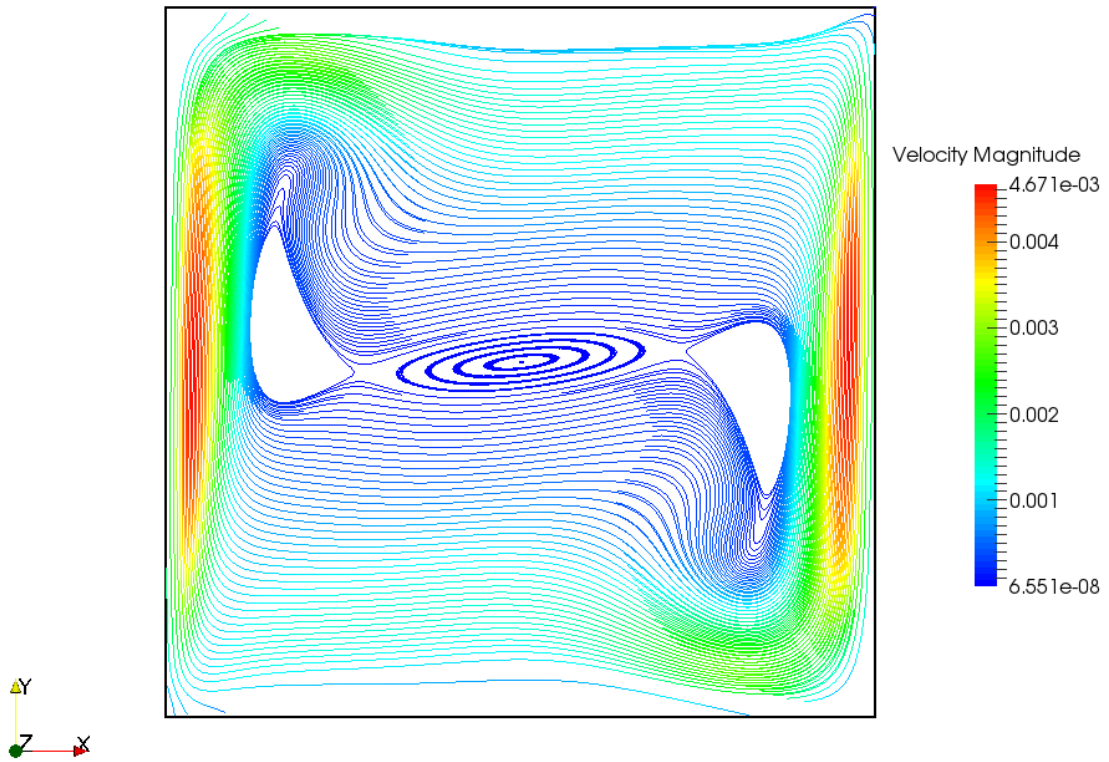


Figure II.25: Streamlines coloured by velocity magnitude.

Chapter III

Part 2 - Data Analysis with user subroutine

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The first part of the tutorial describes how to setup the heated cavity case so that it can be compared directly to published benchmark results. In the second part of the tutorial, we illustrate how users may introduce their own source code in order to calculate additional data of specific relevance to their case based on variables internal to code_saturne and whilst the calculations are running.

1 What you will learn

Through section III, you will learn how:

- code_saturne gives access to all the internal variables which are used in the calculations, whether related to the domain geometry, such as the cells' positions, or the physical properties or the primitive variables for the calculations, such as density or velocity
- User subroutine 'cs_user_extra_operations.c' provides an entry point to use or modify these variables at each iteration or time step
- 'cs_user_extra_operations.c' may be programmed to calculate new, custom variables which are of significance to your case based on the code's internal variables
- To format and add the results to the 'listing' file for clean outputs
- To post-process the output to produce files which can be used easily to produce line plots

2 Comparing the Results with Available Data

We would now like to perform quantitative comparisons with the benchmark results [5, 6] and compare the maximum x and y velocities at the half-way planes and the Nusselt numbers computed at the hot wall and in the vertical mid-plane to the published values. Computing these quantities at each time step will also give us a good indication of the convergence of the calculations.

For $R_a = 10^6$, de Vahl Davis et al. [5, 6] report:

- $\tilde{U}_{x,max} = 64.63$ at $\tilde{x} = 0.5$ and $\tilde{y} = 0.85$
- $\tilde{U}_{y,max} = 219.36$ at $\tilde{x} = 0.0379$ and $\tilde{y} = 0.5$
- $N_{u,0} = 8.817$ at $\tilde{x} = 0.0$, integrated from $\tilde{y} = 0.0$ to $\tilde{y} = 1.0$
- $N_{u,\frac{1}{2}} = 8.799$ at $\tilde{x} = 0.5$, integrated from $\tilde{y} = 0.0$ to $\tilde{y} = 1.0$

where the symbol \sim has been used to denote non-dimensional quantities. In [5, 6], these are defined as follows:

$$\tilde{T} = \frac{T - T_c}{T_h - T_c}, \quad \tilde{u} = \frac{uL}{\kappa} = \frac{\rho C_p}{k} uL, \quad \tilde{x} = \frac{x}{L}, \quad \tilde{y} = \frac{y}{L}$$

In the calculations quoted by [5], [6], the full Boussinesq model is used in which the density is assumed to be constant and its variation with temperature is taken into account only in the buoyancy term. For consistency, we use the density at the cold wall temperature as the reference value and specify the non-dimensional velocity vector as: $\tilde{u} = \frac{\rho_c C_p}{k} uL$.

The Nusselt number, N_u , is evaluated along vertical planes from the definitions:

$$N_u = \int_0^1 \tilde{Q}(\frac{1}{2}, \tilde{y}) d\tilde{y} \quad \tilde{Q} = \tilde{u}_x \tilde{T} - \frac{\partial \tilde{T}}{\partial \tilde{x}} \quad (\text{III.1})$$

Expressed in dimensional variables and applied at the mid-plane ($\tilde{x} = \frac{1}{2}$), this definition becomes:

$$\begin{aligned}
 N_{u, \frac{1}{2}} &= \int_{y=0}^{y=L} \left(\frac{\rho_c C_p}{k} L u_x \frac{T - T_c}{T_h - T_c} - \frac{L}{T_h - T_c} \frac{\partial T}{\partial x} \right) \frac{dy}{L} \\
 &= \frac{1}{T_h - T_c} \int_{y=0}^{y=L} \left(\frac{\rho_c C_p}{k} u_x (T - T_c) - \frac{\partial T}{\partial x} \right) dy
 \end{aligned} \tag{III.2}$$

In discretised form on the computational mesh, the integral in Eq.III.2 will be calculated as a sum of piecewise constant values on all the mesh faces and over the height of the mid-plane.

$$\begin{aligned}
 N_{u, \frac{1}{2}} &= \frac{1}{T_h - T_c} \sum_{y=0}^{y=L} \left(\frac{\rho_c C_p}{k} u_x (T - T_c) - \frac{\partial T}{\partial x} \right)_f \Delta y \\
 &= \frac{1}{T_h - T_c} \sum_{y=0}^{y=L} \left(\frac{\rho_c C_p}{k} u_x (T - T_c) - \frac{\partial T}{\partial x} \right)_f \frac{S_f}{\Delta z} \\
 &= \frac{1}{(T_h - T_c) \Delta z} \sum_{y=0}^{y=L} \left[S_f \left\{ \frac{\rho_c C_p}{k} (u_x)_f (T - T_c)_f - \left(\frac{T_{if2} - T_{if1}}{x_{if2} - x_{if1}} \right)_f \right\} \right]
 \end{aligned} \tag{III.3}$$

where the subscript f indicates a face value, $F_{m,x} = (\rho \bar{u} \bullet \bar{S}_f) n_x$ represents the mass flux through the cell face in the X direction, and Δz is the mesh thickness in the Z direction. The temperature derivative is evaluated with a central-difference formulation across the two cells on each side of the interface, as schematised in Figure III.1 below.

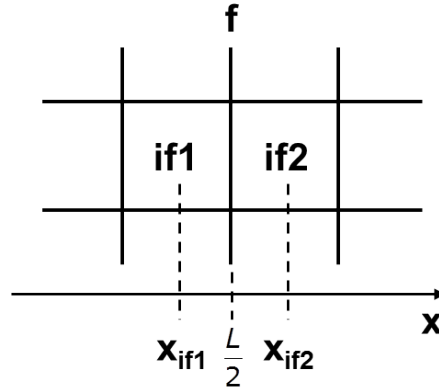


Figure III.1: Mesh cell face schematic.

The density, temperature, and velocity at the cell faces are not stored quantities in code_saturne. Therefore, they must be calculated. In this tutorial which makes use of a uniform mesh, the properties are calculated as means across the cell face whilst the velocity is extracted from the face density and the mass flux:

$$\rho_f = \frac{\rho_{if2} + \rho_{if1}}{2} \quad U_{x,f} = \frac{(\rho \bar{u} \bullet \bar{S}_f) n_x}{\rho_f} = \frac{F_m n_x}{\rho_f} \tag{III.4}$$

The mass flux through the face, $F_{m,x} = (\rho \bar{u} \bullet \bar{S}_f) n_x$, is one of the stored variables at boundary and internal faces which are available in 'cs_user_extra_operations.c'.

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For the Nusselt number along the hot wall, the expression simplifies to:

$$\begin{aligned}
 N_{u,\frac{1}{2}} &= \frac{1}{T_h - T_c} \int_{y=0}^{y=L} \left(-\frac{\partial T}{\partial x} \right) dy \\
 &= \frac{1}{(T_h - T_c)\Delta z} \sum_{y=0}^{y=L} \left[S_f \left\{ -\left(\frac{T_i - T_b}{x_i - x_b} \right) \right\} \right] \\
 &= \frac{-1}{(T_h - T_c)\Delta z} \sum_{y=0}^{y=L} \left[S_f \left\{ \frac{T_i - \text{coefap}(b)}{x_i - x_b} \right\} \right]
 \end{aligned} \tag{III.5}$$

The temperature at each boundary face is computed based on code_saturne 's 'coefap' boundary conditions definition array.

The implementation of the formulae in the user-defined subroutines is described next.

3 Customising 'cs_user_extra_operations.c'

Similar to the steps described in Section II for 'cs_user_physical_properties.c', start by copying:

/HeatedSquareCavity/Rayleigh1Million/SRC/REFERENCE/cs_user_extra_operations.c

to your local SRC directory:

/HeatedSquareCavity/Rayleigh1Million/SRC/.

to create a local copy which you will be able to customise and which will be automatically recompiled and linked with the 'cs_solver' executable at run time.

The customised code available with the tutorial is already commented. Here we describe the main parts and the logic behind them.

1. Declare your own local variables at the top, as double precision real values or integer.
2. Collect information about the case, geometrical and physical. This makes the subroutine setup independent and flexible:
 - (a) Identify wall faces
 - (b) Find their position and the temperature which has been ascribed to them
 - (c) From their position, compute the size of the domain (assumed to be of square shape) and the position of the vertical and horizontal mid-planes
3. Compute the Nusselt number for the left vertical wall by cycling through the faces for that wall, identified using a combination of wall-boundary face indices and their boundary condition
4. Compute the Nusselt number and the maximum x-axis velocity in the vertical mid-plane
 - (a) Cycling through the internal faces, identify the faces which join cells on each side of the mid-plane. Because of inevitable numerical inaccuracies, this is more reliable than finding faces which are exactly at the mid-plane.
 - (b) Compute the face values of density, temperature and velocity
 - (c) Compute the face contribution and accumulate the Nusselt number
 - (d) Compute the maximum x-axis velocity, store its non-dimensional value and its location
5. Compute the maximum y-axis velocity in the horizontal mid-plane
 - (a) Cycling through the internal faces, identify the faces which join cells on each side of the mid-plane. Because of inevitable numerical inaccuracies, this is more reliable than finding faces which are exactly at the mid-plane.

- (b) Compute the face value of density and velocity
 - (c) Compute the maximum y-axis velocity, store its non-dimensional value and its location
6. Output the Nusselt numbers, and the maximum velocities and their locations in adimensional form in the 'listing' file. The output is formatted and uses the keyword 'us_extraops' to flag the data in 'listing'.

4 Running the case

To run the case, simply repeat the calculations that are described in Section II. 'cs_user_extra_operations.c' will automatically be detected, compiled and linked with the code_saturne executable.

At the end of the calculation, open the 'listing' file and look for the keyword 'us_extraops'. Data should appear as below:

```

** Heated Cavity Solution **
-----
-----
      Iter   Nu_mid     Nu0      Ux_max     y(Ux_max)   Uy_max     x(Uy_max)
      1       0      0.1554E+03      0      0.00625      0      0.00625
-----
-----

```

Figure III.2: Output from 'cs_user_extra_operations.c', after 1 iteration.

```

** Heated Cavity Solution **
-----
-----
      Iter   Nu_mid     Nu0      Ux_max     y(Ux_max)   Uy_max     x(Uy_max)
      450    1.6422E+01  0.9162E+01  0.6635E+02  0.8563E+00  0.2209E+03  0.3125E-01
-----
-----

```

Figure III.3: Output from 'cs_user_extra_operations.c', after 450 iterations.

Aside from direct, quantitative comparisons with existing data, computing representative variables for a case is also very useful to evaluate calculation convergence and stability. For example, in Linux you may use the command:

```
grep -n us_extraops ../listing > HeatedSquareCavity.txt
```

which will output all the data in the text file specified. The file may then be edited to remove 'us_extraops' and line numbers and imported in a plotting package to graph the evolution of all the variables as a function of the number of iterations.

5 Comparison with Benchmark Data

The calculated values at the last iteration (450) are compared with the published data in Table III.1 below, showing an excellent quantitative agreement.

	$Nu_{\frac{1}{2}}$	Nu_0	\tilde{u}_{\max}	\tilde{y}_{\max}	\tilde{v}_{\max}	\tilde{x}_{\max}
code_saturne	8.99	8.99	65.12	0.86	218.7	0.0313
Benchmark	8.8	8.82	64.63	0.85	219.36	0.0379
Error (%)	2.16	1.93	0.76	1.2	-0.3	17.4

Table III.1: Comparison between code_saturne 's and the benchmark results.

The error is larger for the position of the maximum Y-axis velocity in the horizontal mid-plane. However, the benchmark maximum values were obtained by fourth-order interpolation whereas here they are taken at the centre of the cell faces. The absolute difference between the code_saturne and benchmark value is equal to $0.0379 - 0.0313 = 6.6 \times 10^{-3}$, which is less than the interval size between two cell centres, $\Delta\tilde{x} = \frac{1}{L} \frac{L}{80} = 1.25 \times 10^{-2}$, and shows that the location of the maximum is captured accurately in code_saturne.

To test your code, you are encouraged to repeat the tests for the lower values of $R_a = 10^4, R_a = 10^5$ which are also listed in [5, 6].

Chapter IV

References

1 References

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Chapter V

Appendix

1 Appendix A – How to create the computational domain

The computational domain is created with the Shaper module of SALOME. As the geometry is the same as for tutorial [7] (shear driven 2D cavity), in what follows the geometry creation will be referring to this tutorial and only the elements which differ from the setup of Tutorial 0 will be highlighted. Therefore, if you are not already familiar with Shaper, you should first go through Tutorial 0 [7]. **Note** : Another technical meshing option could be consider via the *Generate cartesian mesh* option in code_saturne. See II.4.

1.1 Geometry

Follow the same procedure as explains in [7]:

- Create a thin box of dimensions 1.0 m x 1.0 m x 0.01 m
- Create groups including faces and edges to simply boundary conditions settings

This time you need to create groups entitled *Adiabatic_Walls*, *Hot_Wall* and *Cold_Wall* and *Symmetry_Walls* based on II.1. See the following figure.

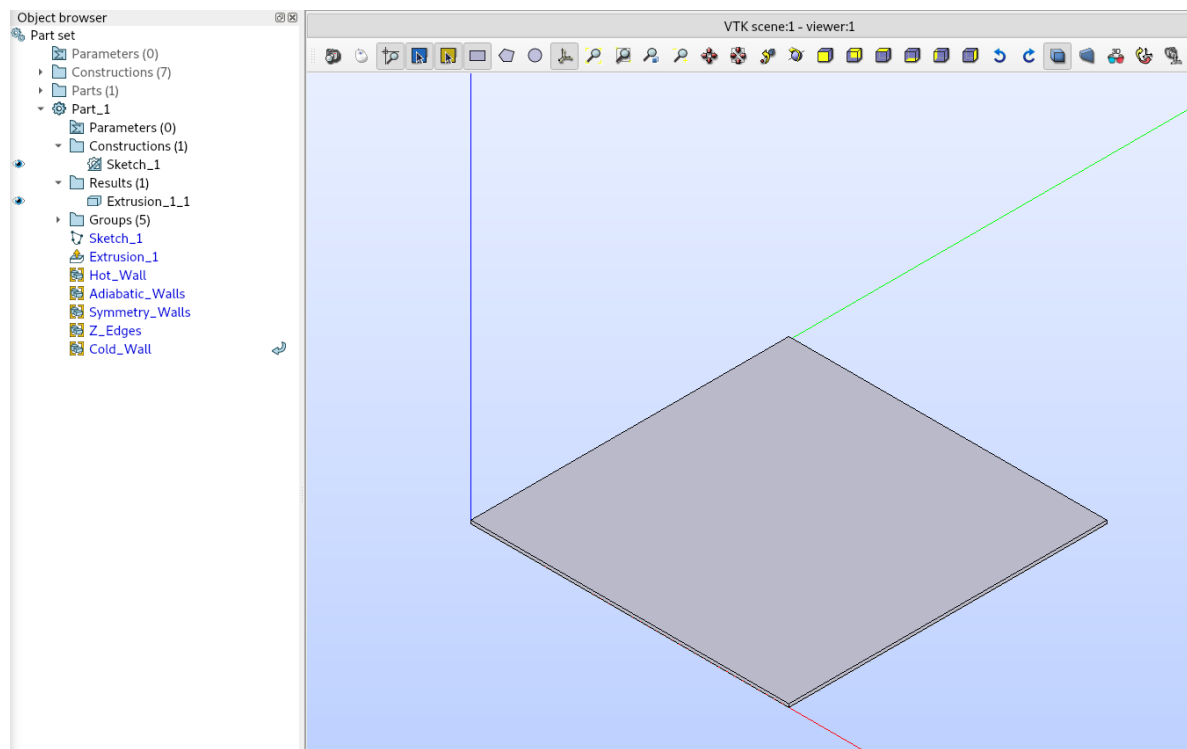


Figure V.1: Groups

You could save the file as *HeatedSquareCavity* before moving to Meshing procedure.

If your results are like Figure ??, '*HeatedSquareCavity*' is now ready to be meshed. Save the file and proceed to Meshing.

1.2 Meshing

Switch to the meshing module, which opens the 'VTK scene viewer'. Create the 'Mesh' and rename it '*HSC_mesh*'. Similarly to Tutorial 0 [7], create a uniform, rectangular mesh with one cell in the Z

direction by following the methodology described in Tutorial 0 [7]. However, this time specify **80 cells** for the discretisation along the 'X' and 'Y' edges, as shown in Figure V.2 below.

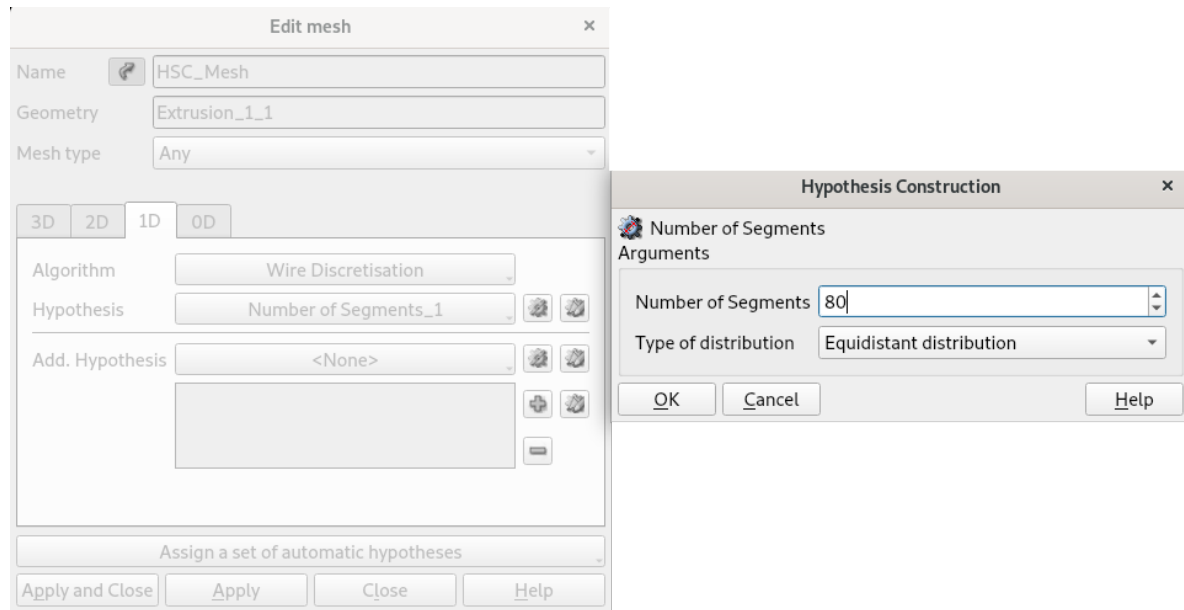


Figure V.2: Edge discretisation for the edges along the X and Y directions.

When all the sub-meshes have been specified, right-click on 'HSC_mesh' and select 'Compute' to generate the mesh.

The mesh is now completed and the different boundaries may be assigned different colours for visualisation, as described in Tutorial 0 [7].

Save the SALOME file and export the mesh file in '.med' format as per the methodology detailed in Tutorial 0 [7]. The file should be placed in the 'MESH' directory of the 'HeatedSquareCavity' study, where code_saturne will expect the file to be situated by default.

For the file name, choose 'HSC_mesh'; the '.med' extension is automatically added. You are now ready to set up the CFD simulation with the CFDStudy module.