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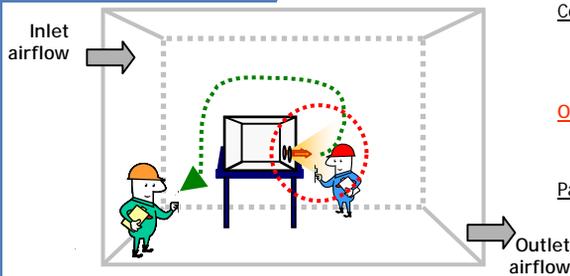
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## Problem approach



**Context:**

To ensure protection of operators working in a ventilated room and to optimize supervision of workspaces, it is necessary to have access to aerosol concentration in every point of this room. The transfer of this contamination is independent of its radioactive properties.

**Objective:**

This study aims at developing a model of aerosol transport and deposition, giving the space-time evolution of the particulate contamination concentration  $C(x, y, z, t)$

**Parameters:**

- aerosol mass median aerodynamic diameter
- aerosol concentration and velocity at emission
- configuration of ventilation
- airflow velocity

## Aerosol transport modelling

### Simplification of the problem:

- very dilute two-phase flow
  - no particle collision or coalescence
- high density of particles ( $\rho_p/d_f \geq 1000$ )
  - Stokes' law can be applied, particle relation time follows the relation:

$$\tau_p = \frac{d_p^2 \rho_p}{18\mu_f} Cu$$

→ phenomena such as pressure gradient force, virtual mass force or lift force can be neglected.

### Formulation of the transport model:

Airflow is simulated with RANS method with k- $\epsilon$  turbulence model or  $R_{ij}$ - $\epsilon$  turbulence model.

Particles (dispersed phase) are simulated with a simplified Eulerian model, called "Diffusion-Inertia Model" (Zaichik et al., 2004). It contains a single transport equation of particle concentration:

$$\frac{\partial C}{\partial t} + \frac{\partial}{\partial x_i} \left\{ U_{f,i} + \tau_p g_i - \tau_p \left( \frac{\partial U_{f,i}}{\partial t} + U_{f,k} \frac{\partial U_{f,i}}{\partial x_k} \right) \right\} C$$

$$= \frac{\partial}{\partial x_i} \left[ \left( D_B \delta_{ik} + D_{p,ik}^t \right) \frac{\partial C}{\partial x_k} + C \frac{\partial}{\partial x_k} \left( D_B \delta_{ik} + \frac{\Omega}{1+\Omega} D_{p,ik}^t \right) \right]$$

Labels in diagram: sedimentation, particle deviation from streamlines, Brownian and turbulent dispersion, migration due to thermophoresis and turbophoresis.

The model accounts for Brownian diffusion. But in most of cases, Brownian effects are negligible comparing to turbulent effects.

## Aerosol deposition modelling

### Deposition models

In this study, deposition laws in diffusion and gravitational regime have to be considered ( $0.1 \mu\text{m} < d_p < 50 \mu\text{m}$ ).

- two categories of models

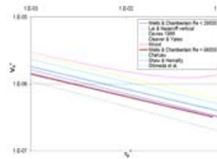
→ semi-empirical laws:  $v_d^+ = k_1 S c^{k_2} + \delta v_s^+$

→ theoretical laws:

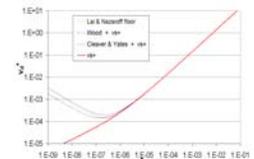
$$v_d^+ = \frac{1}{I_f} \quad v_d^+ = \frac{v_s^+}{1 - \exp(-v_s^+ I_f)} \quad v_d^+ = \frac{v_s^+}{\exp(v_s^+ I_f) - 1} \quad I_f = \int_{d_f/2}^{30} \left( \frac{v_f}{v_f + D_B} \right) dy^+$$

Labels: vertical surfaces, upward surfaces, downward surfaces

- comparison of deposition laws



Horizontal surface



Upward surface

## Simulations

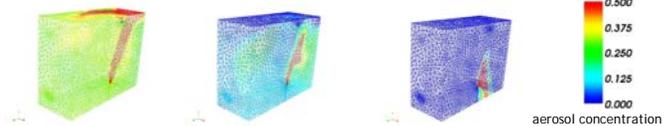
The Diffusion-Inertia model and deposition laws have been implemented in *Code\_Saturne*, an open-source free software CFD code, developed by EDF R&D.

First simulations of aerosol dispersion in a ventilated room ( $36 \text{m}^3$ ):

$d_p = 2 \mu\text{m}$ :

$d_p = 20 \mu\text{m}$ :

$d_p = 50 \mu\text{m}$ :



aerosol concentration

Validations on simple geometries are currently carried out (sedimentation channel, cylindrical ducts, bent tubes) in parallel.

## Conclusion

Preliminary bibliographical researches allowed to identify transport and deposition models, and to test them with first calculations using *Code\_Saturne*. Tracing experiments carried out in a  $36 \text{m}^3$  room are intended to validate these models in ventilated room, with different configurations of ventilation.

In order to improve the precision in aerosol deposition results, and also to obtain deposition results independent of meshes used, a method establishing the aerosol concentration profile in the near-wall region is currently developed.



Experimental facility CEPIA ( $36 \text{m}^3$ )