

Club des Utilisateurs de *Code_Saturne*

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Droplet Breakup by a Plasma Jet

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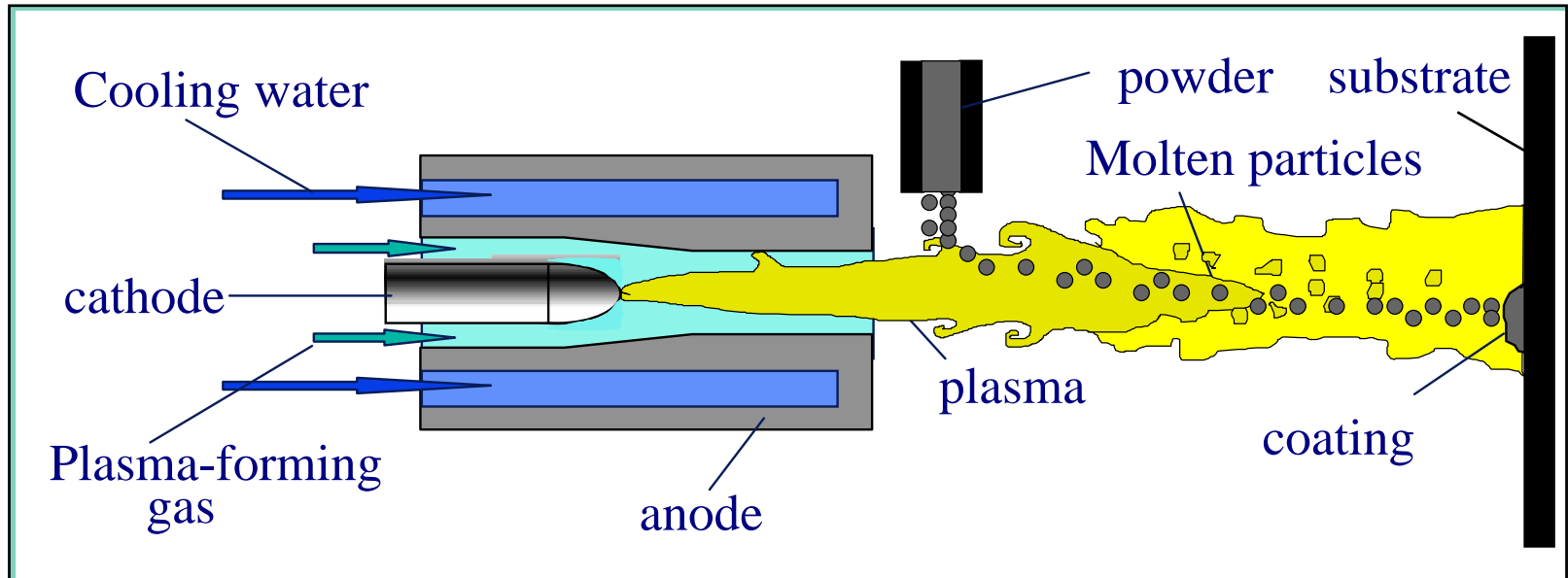
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Conventional Powder Plasma Spraying



Plasma with high velocity ($> 1\ 000\ \text{m.s}^{-1}$) and high temperature ($T > 10\ 000\ \text{K}$)



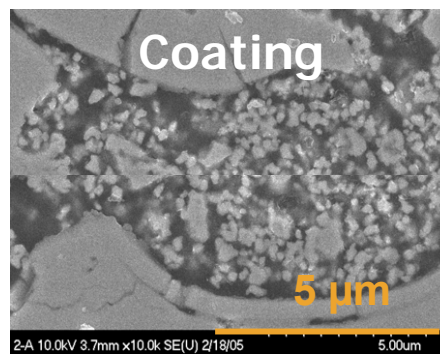
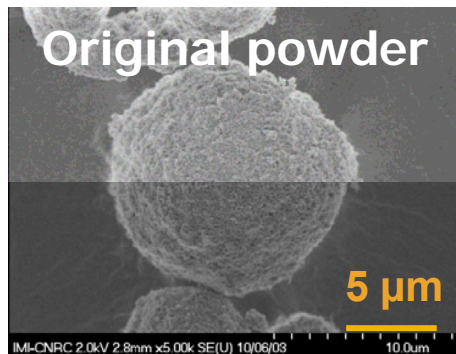
Micro-structured coatings

Nano-structured Coatings by Plasma Spraying

Better mechanical properties of nano-structured coatings

Solid feedstock : powders

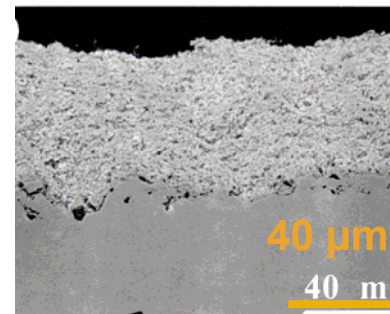
Spraying of agglomerates of nano-size particles



R. Lima, B. Marple
JTST, 16(1), 2007, pp 40-63

Liquid feedstock

Use of stable and homogeneous liquid feedstock with a low viscosity



M. Gell et al, SCT, 183,
2004, pp 51-61

Liquid Precursor Plasma Spraying

Two main difficulties:

❶ **Injection and penetration** of the liquid into the plasma flow

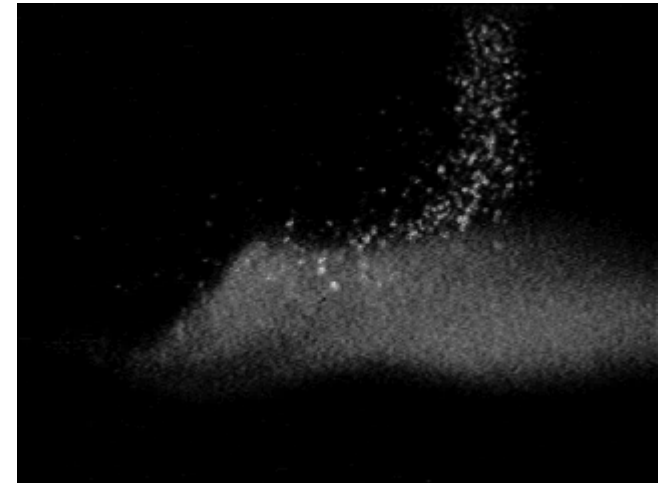
Penetration: $\rho_l v_l^2 \geq \rho v^2$

❷ **Heterogeneous behavior** of the droplets
in the core and periphery of the plasma jet

Similar problems in conventional
powder plasma spraying

But with liquid feedstock, they are
aggravated because of:

- the low specific density of droplets
- the breakup process



Injection of Mo particles
in Ar-H₂ plasma jet

Droplet Breakup Processes under Plasma Conditions

- **Aerodynamic Breakup**

 - Secondary breakup*

 - High relative velocity at the interface of two phases

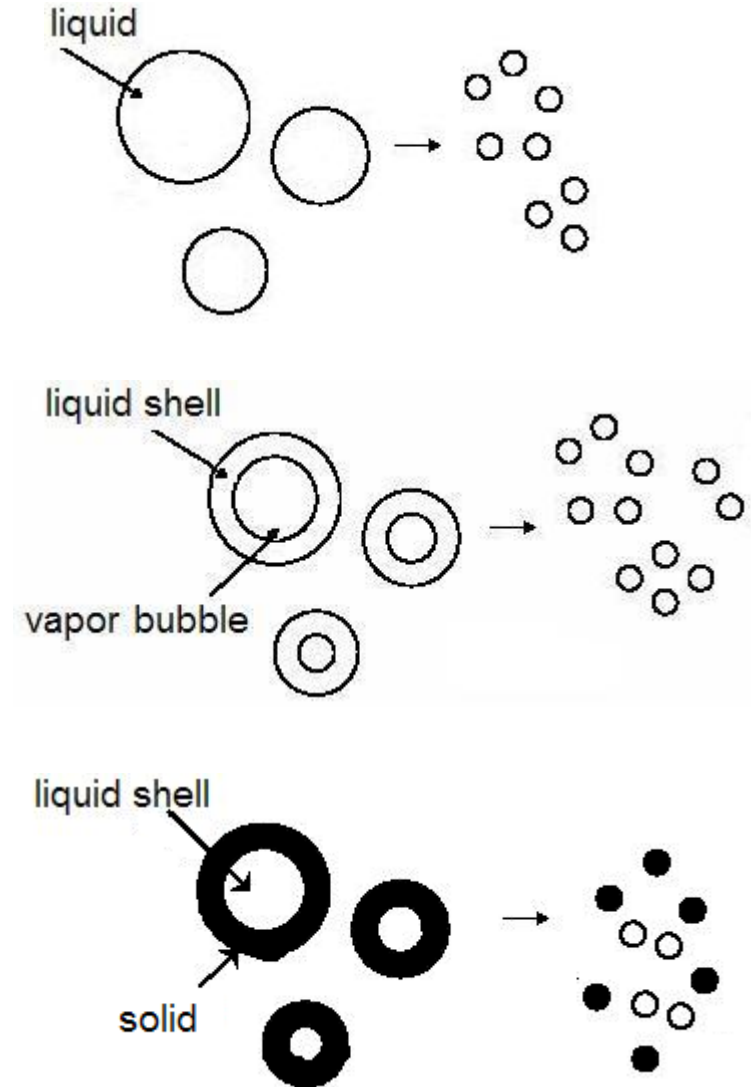
- **Thermal Breakup**

 - Inner boiling of liquid

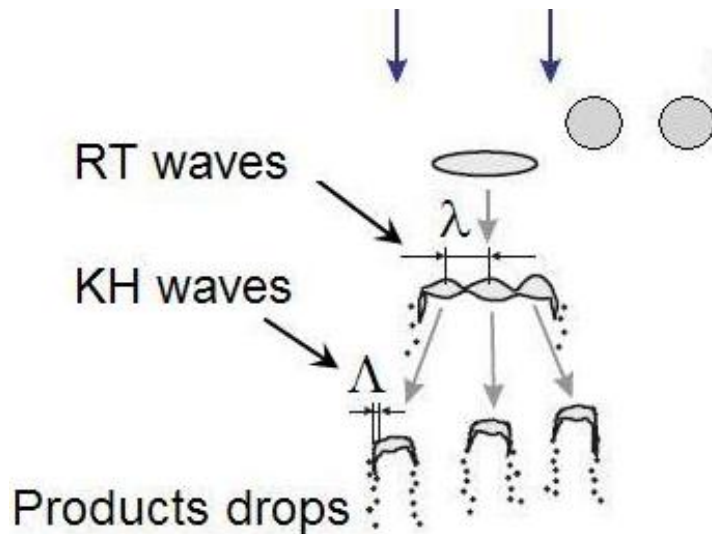
- **Liquid droplet: Sphere rupture**

 - Formation of solid shells

 - + pressurization of inner liquid



Aerodynamic Droplet Fragmentation



Breakup results from:

- **Rayleigh-Taylor instabilities:**
density difference
- **Kelvin-Helmholtz instabilities:**
velocity difference

$$\rho_{\text{plasma}} (1000 \text{ K}) \sim 0.4 \text{ kg.m}^{-3} / \rho_{\text{water}} \sim 1000 \text{ kg.m}^{-3}$$

$$v_{\text{plasma}} (1000 \text{ K}) \sim 1000 \text{ m.s}^{-1} / v_{\text{water}} \sim 30 \text{ m.s}^{-1}$$

Hwang & al., Atomisation & sprays, 6, 1996

Weber dimensionless number

$$We = \frac{\rho \Delta U^2 d}{\sigma}$$

fluid's inertia

surface tension

ρ : fluid density

ΔU : velocity difference between
plasma and droplet

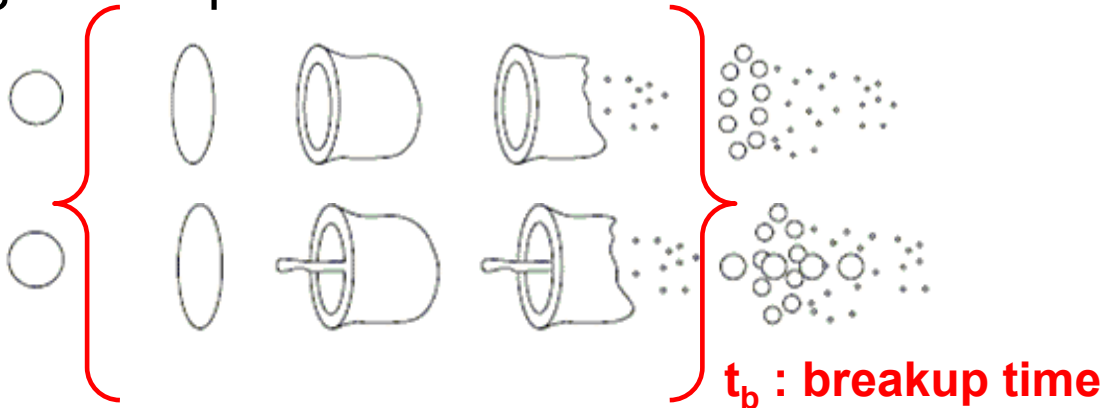
d : droplet diameter

σ : surface tension

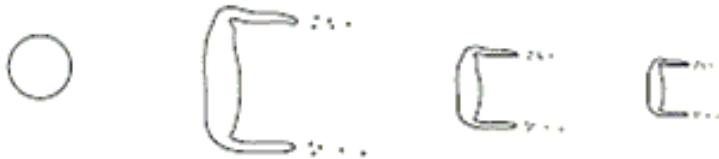
Fluid momentum flux

Aerodynamic Breakup Regimes

Bag breakup: $We < 100$



Stripping (shear): $100 \leq We < 350$



Catastrophic (surface wave) breakup: $We \geq 350$



Models

TAB Model
for low We
O'Rourke, 1987

ETAB Model
Tanner, 1998

Wave Model
for $We > 100$
Reitz, 1982

ETAB Model

$$\frac{dn(t)}{dt} = 3K_{br}n(t) \implies n(t) = e^{3K_{br}t}$$

- We ≤ 160: $K_{br} = k_1\omega$
 - We > 160: $K_{br} = k_2\omega\sqrt{We}$

$$\bar{m}(t) = m_0/n(t)$$

r : droplet radius
 n(t) : number of product droplets
 m : droplet weight
 K_{br} : proportionality constant
 ω: instability growth rate
t : breakup time

	Experimental conditions used for validation of ETAB Model (Schneider, 1995)	Operating conditions for the injection of liquid in the plasma jet
Liquid feedstock	Fuel	Solution: Dissolved metal salt in water
Injection	P_{injection} = 300 bars d₀ ~ d_{injector} = 150 μm v₀ = 183 m.s⁻¹	P_{injection} ~ 5 bars d₀ ~ d_{injector} = 300 μm v₀ ~ 30 m.s⁻¹
Atmosphere	N₂ P_{N2} = 15 bars ρ_{N2} = 12.7 kg.m⁻³	Plasma gas T_{plasma} = 300 K – 10 000 K ρ_{plasma} < 1 kg.m⁻³

Modeling the Turbulent Flow outside the Plasma Torch

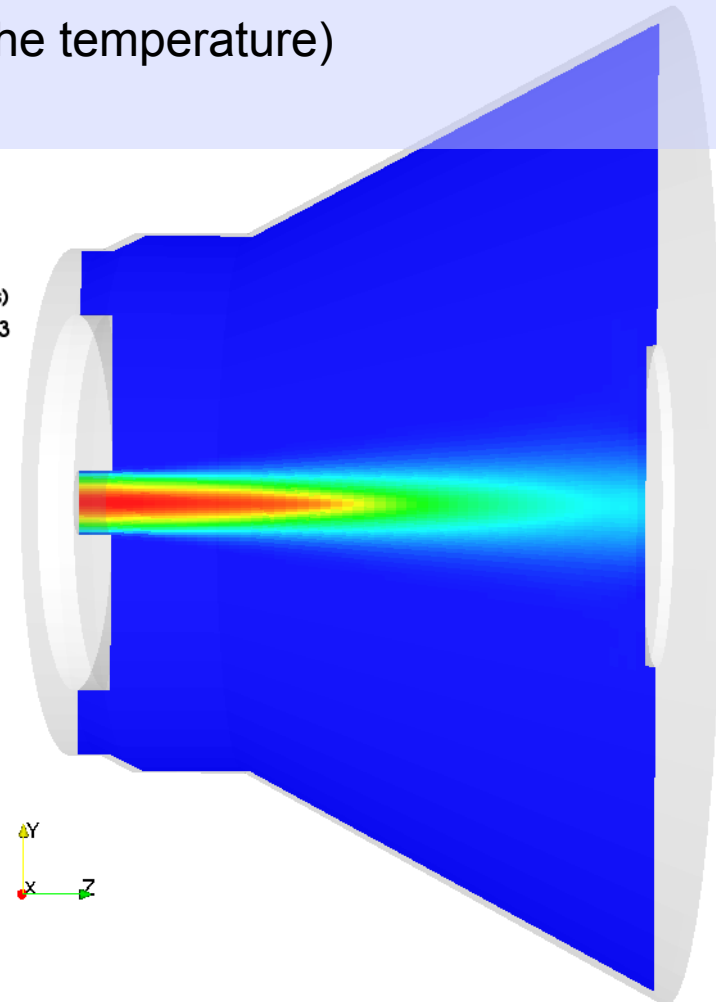
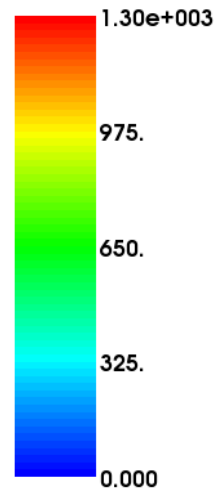
Main assumptions

- 3-D geometry
- 2 gases : plasma (Ar-H₂) and ambient air (no demixion and chemical reactions)
- Mixing laws to calculate properties (dependant on the temperature)
- Turbulent flow outside the plasma torch : k- ϵ

Plasma torch operating conditions

- Torch nozzle diameter: 6mm
- Velocity profile
($v_{max} = 1300 \text{ m.s}^{-1}$)
- Temperature profile
($T_{max} = 13400 \text{ K}$)

Gas velocity (m/s)



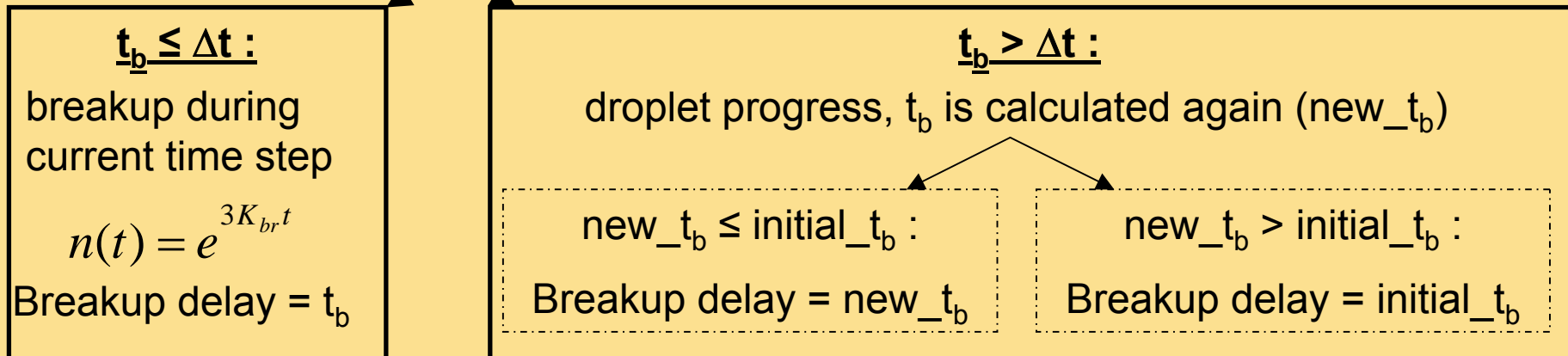
Modeling the Liquid Penetration on the Plasma Jet

Main assumptions

- Spherical, punctual and pure liquid droplets (no interactions between droplets)
- Droplets ($\phi = 300 \mu\text{m}$, $v_0 = 30 \text{ m.s}^{-1}$) subjected to the fluid turbulent dispersion
- Phenomenon: aerodynamic breakup only (no thermal effects or evaporation)

ETAB Model Breakup

We ≥ 12 : breakup possible \rightarrow calculation of breakup time t_b

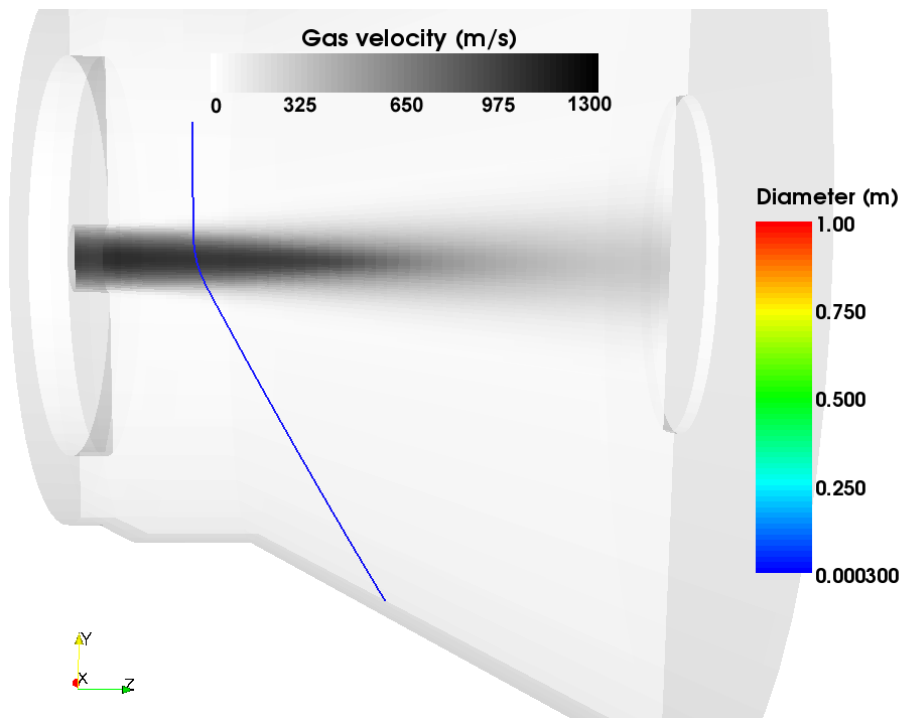


Created droplets with new characteristics at the current time step:
diameter, mass, velocity and trajectory

Comparison of the ETAB Model Result and Experimental Observation

Injection of a liquid 300 μm droplet in the plasma jet

$$k_1 \sim k_2 = 1/4,5$$

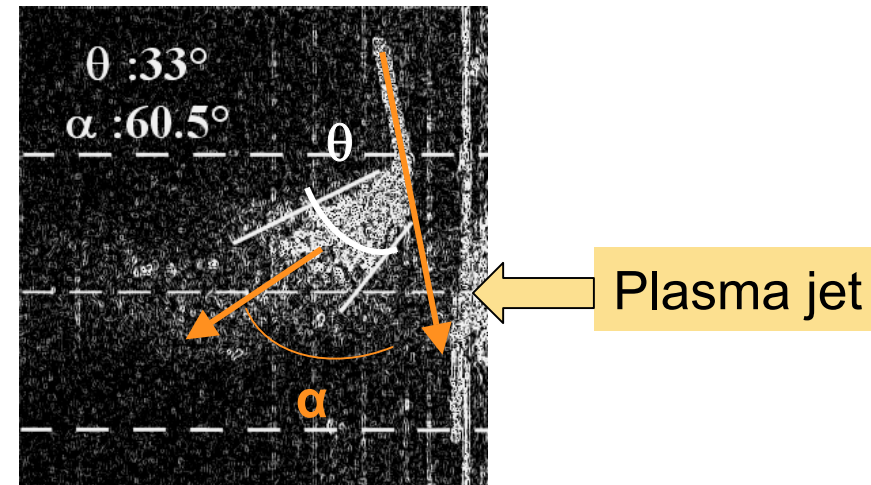


Trajectory of a 300 μm droplet
no breakup

Injection of a liquid jet in the plasma jet

θ : dispersion angle of the liquid spray jet

α : deviation angle of the liquid spray jet

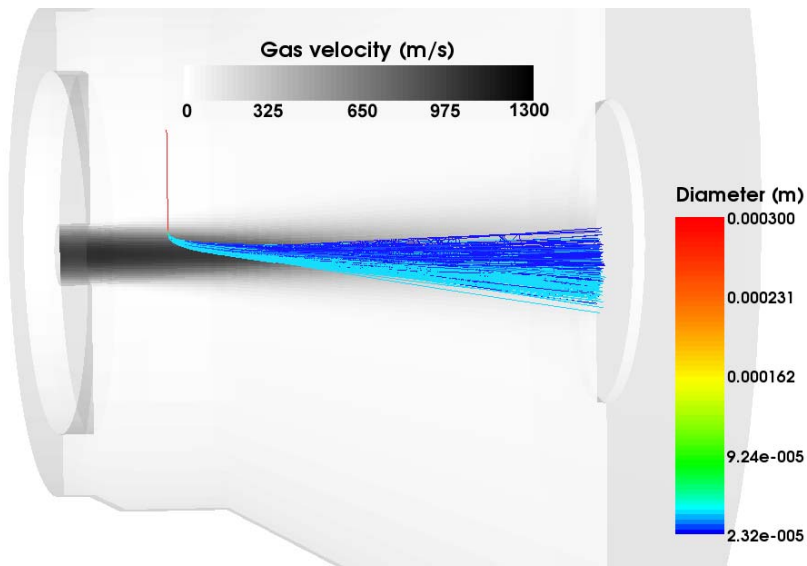


R. Etchart-Salas, V. Rat, J.F. Coudert, P. Fauchais
Université de Limoges, France ITSC 2007

Effect of the k1 Constant on a 300 μm Droplet Breakup

$$n(t) = e^{3K_{br}t} \quad \text{with } K_{br} = k1\omega \text{ (We} \leq 160) \text{ and } t_b = 1/K_{br}$$

k1 = 10

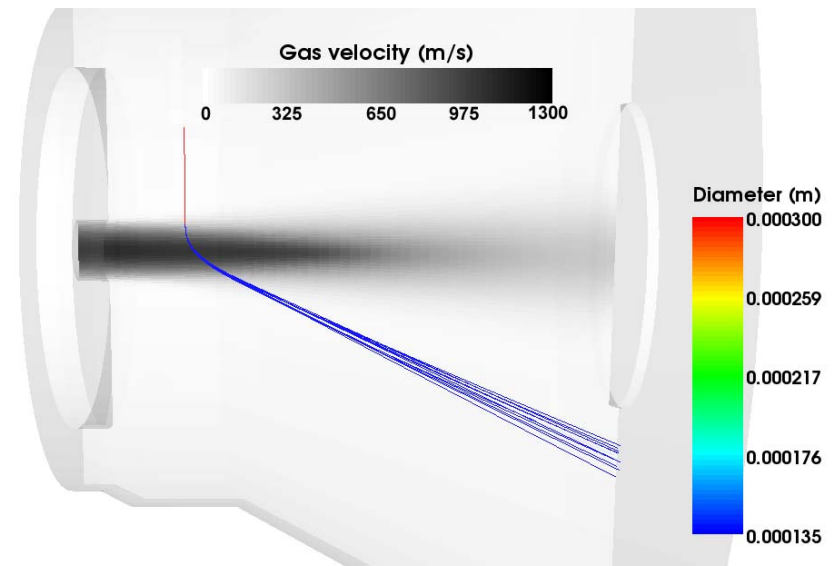


197 breakup → 980 droplets

$t_b \text{ max} = 7.6 \cdot 10^{-6} \text{ s}$

We max = 26.9

k1 = 100



1 breakup → 11 droplets

$t_b \text{ max} = 7.6 \cdot 10^{-7} \text{ s}$

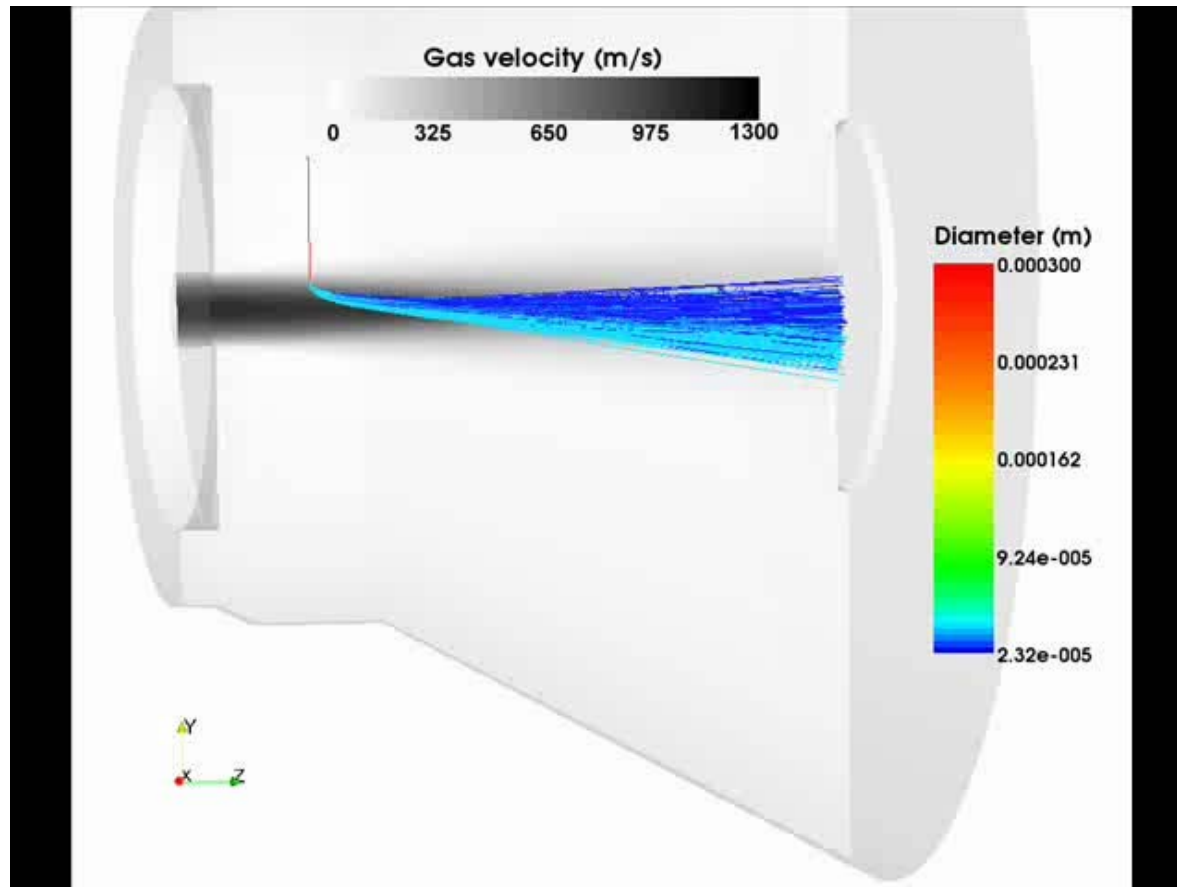
We max = 51.8

Droplets Trajectories

Visualization of 500 droplets maximum

- if number < 500: all droplets display
- if number > 500: maximum different droplets viewed

$k1 = 10 \rightarrow 980$ droplets



Conclusion

Implementation of ETAB model in *Code_Saturne*:

- Qualitative study of droplets breakup
- Influence of the k_1 constant on the droplet breakup and trajectories of new droplets

- Statistic study
- Validation of the implementation of the ETAB model in *Code_Saturne* with simulation of Schneider experiment
- Work in progress to determine appropriated constants to plasma conditions

Thanks for your attention

